

# How to reduce the LCoA of green NH<sub>3</sub> with hybrid CSP-PV plants

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**PacificGreen**  
Solar Technologies



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Technologies Group



**AMMONIA ENERGY**  
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# PGTK Technologies & Company Development

Leading environmental technologies group

## Vision

PGTK’s vision is a world in which the issues of climate heating and resource scarcity are addressed by technological innovation and sensible stewardship

## Mission

PGTK’s mission is to develop and deliver renewable technologies globally

## Development

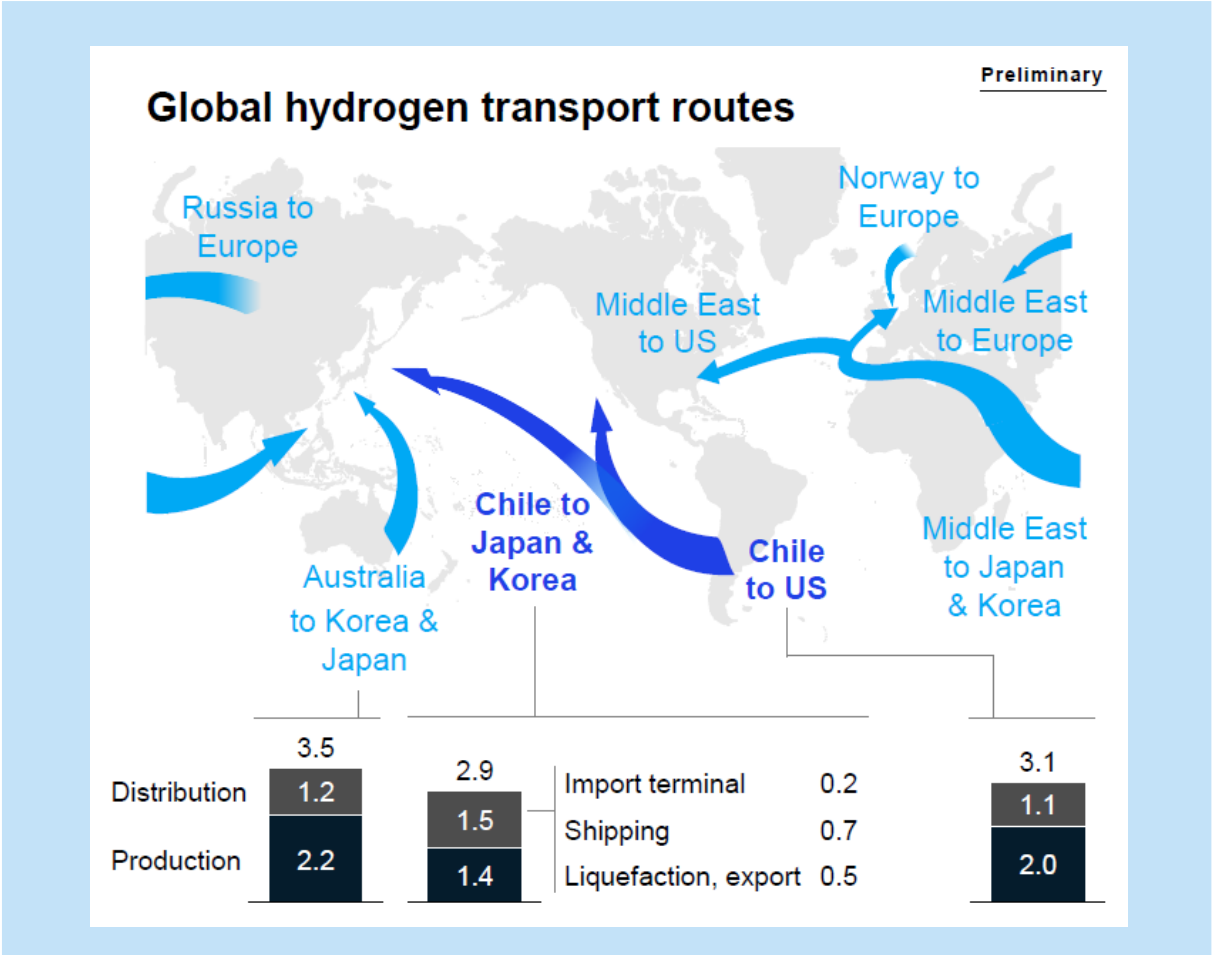
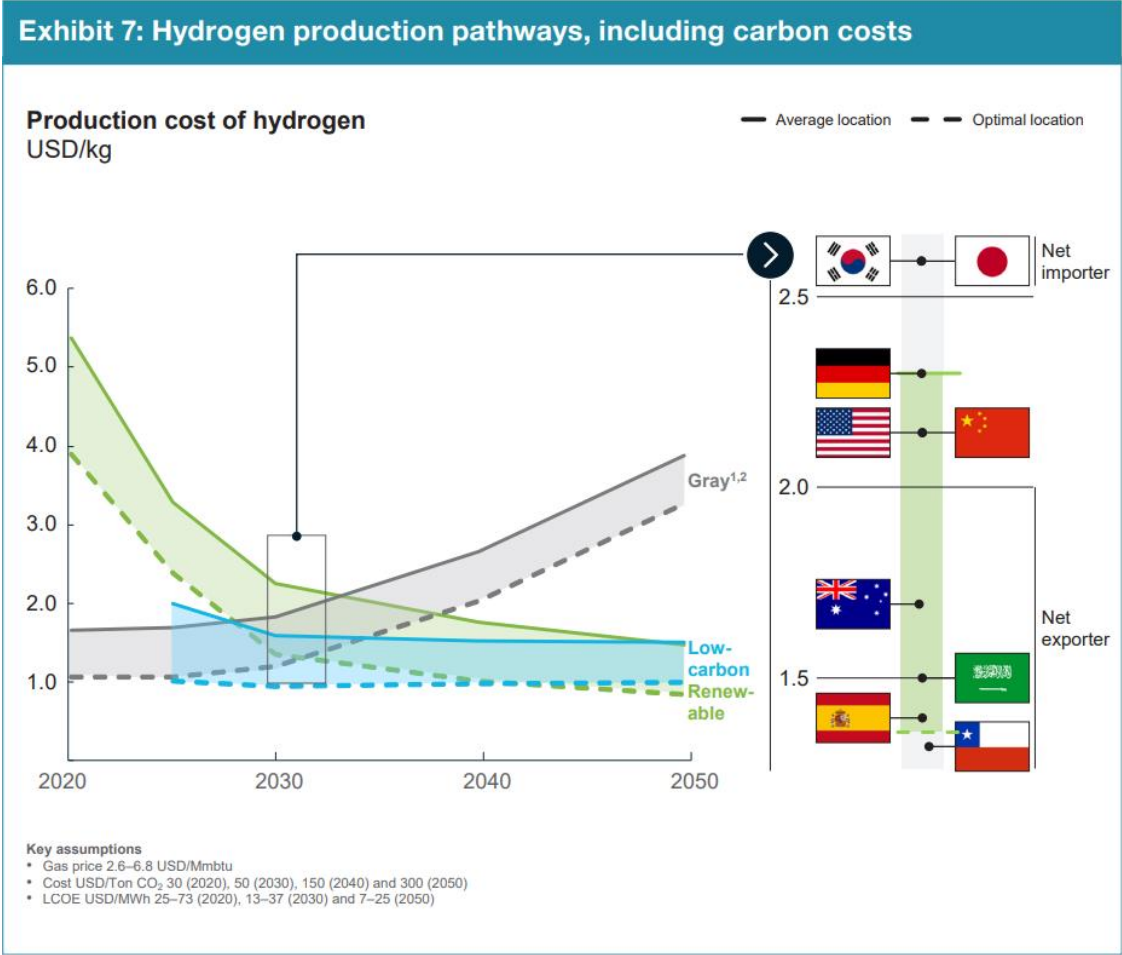
Evolved from a niche technologies development start-up into a globally recognized environmental and renewables group across multiple sectors



### Rapid five-year development across seven different technologies



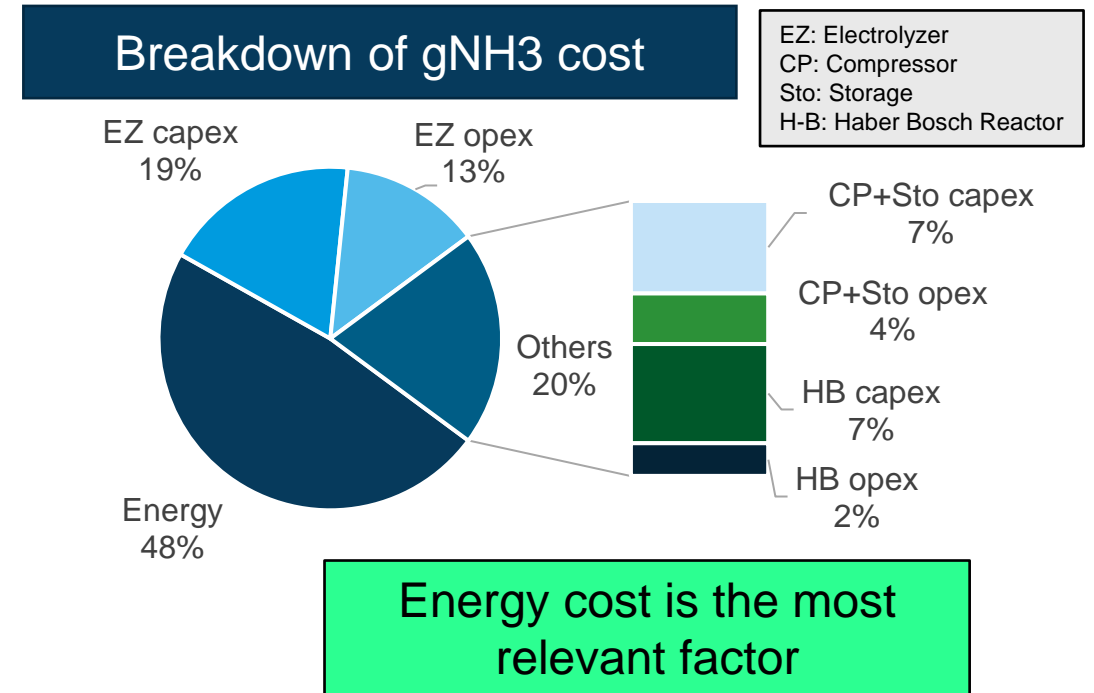
# Context – Huge hype for Green Hydrogen



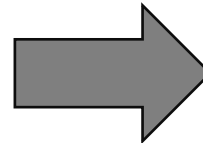
<sup>1</sup> Mckinsey & Company, 2021. Hydrogen Insights, 2021.  
<sup>2</sup> Ministerio de Energía de Chile, “National Green Hydrogen Strategy.”

# Context – From Green Hydrogen to Green Ammonia

- Ammonia production is mainly made by a Haber-Bosch Reactor
- Ammonia is one of the most demanded chemical in the industry
- It has the potential to be used as an energy carrier of the Hydrogen



How to make the H<sub>2</sub> and NH<sub>3</sub>  
Green with Solar?



The best option is  
**PV+CSP technology.**

How a hybrid CSP+PV plant can reduce the LCoA?

What could be the CSP role on gH<sub>2</sub> and gNH<sub>3</sub> industry?

How we design a CSP considering the profile requirements of the ammonia industrial plant?

# System Description – CSP+PV Generation Plant and H2+NH3 Industrial Plant

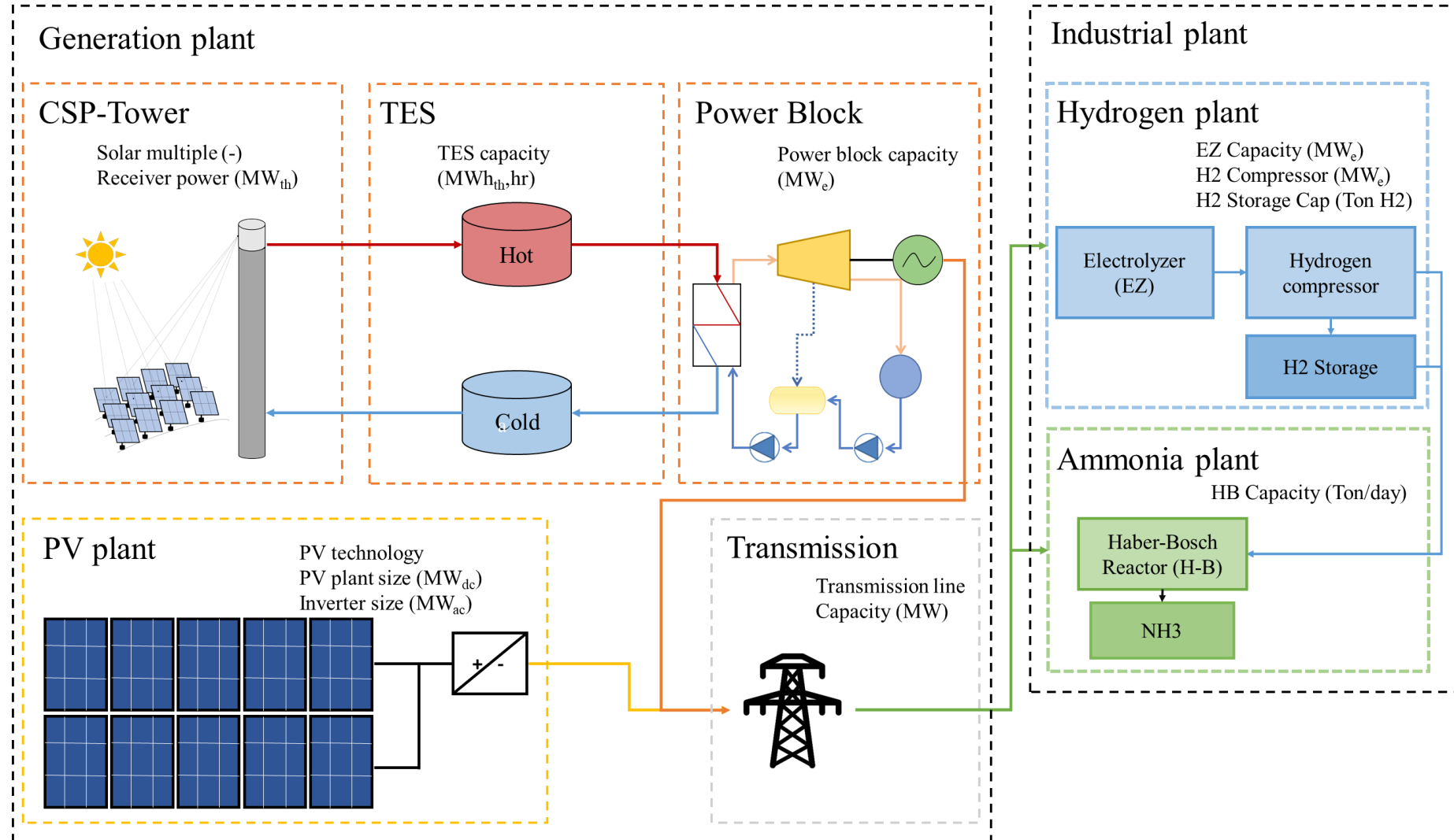
## Main system

### Generation plant:

- CSP Tower [MW]
- PV plant [MW]

### Industrial plant

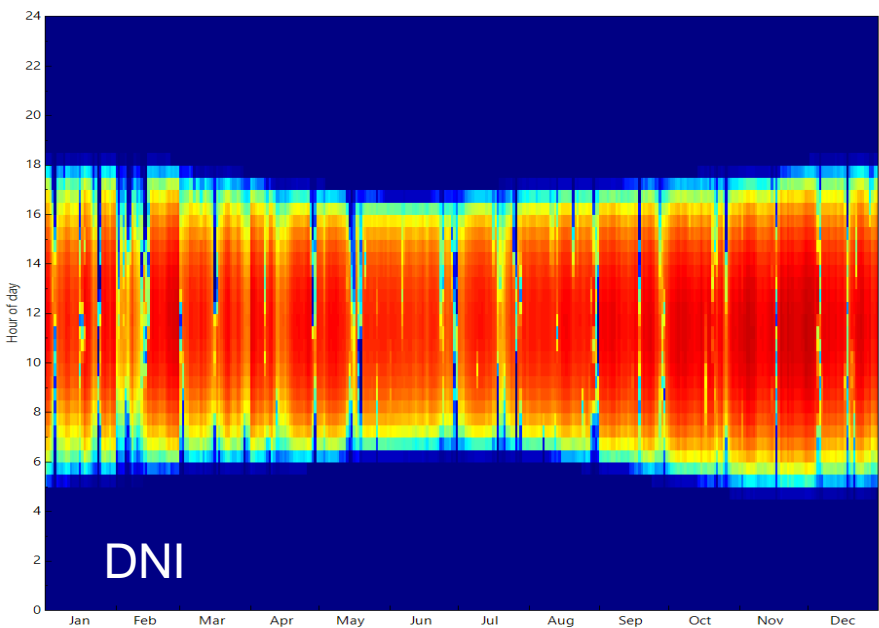
- Electrolyzer [MW]
- H2 Compressor [MW]
- H2 Storage [Ton]
- Haber-Bosch Reactor [Ton/d]



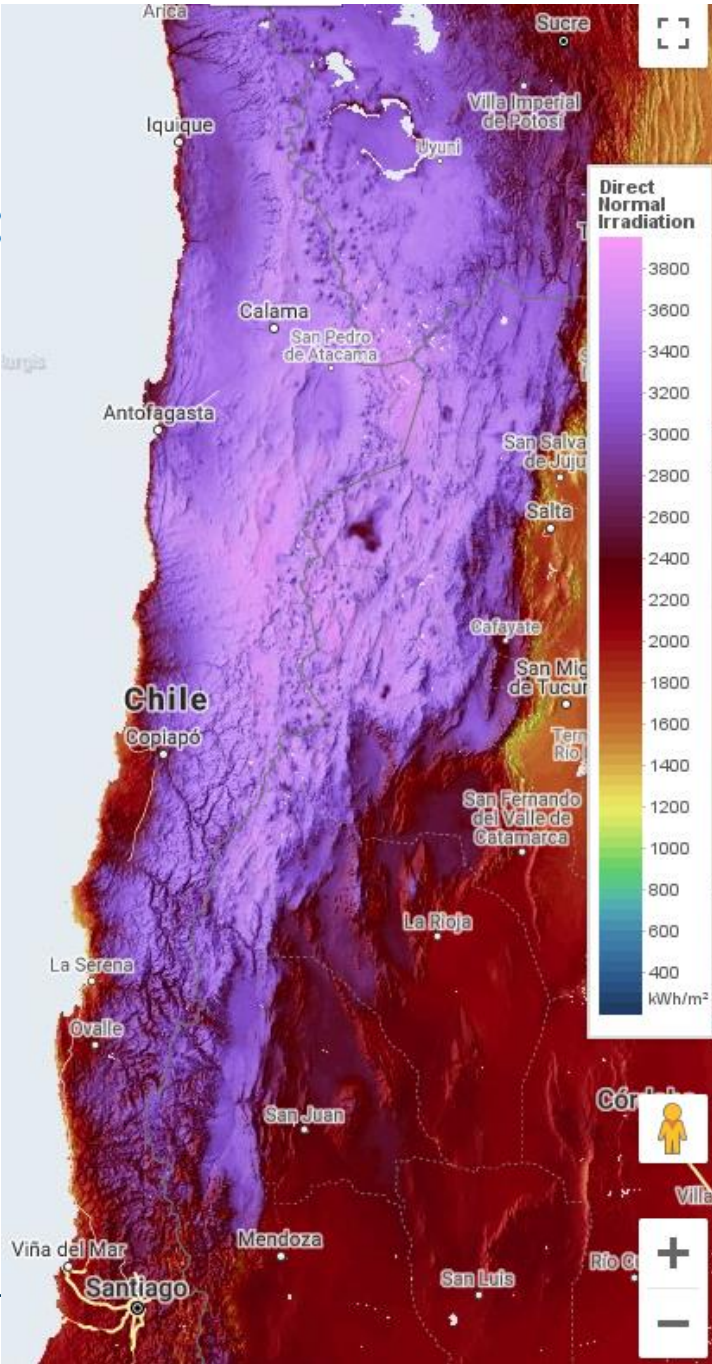


# Case of Study – Chile Atacama Desert

- Analysis performed for northern Chile - Atacama Desert conditions.
  - DNI: **3500** kWh/m<sup>2</sup>-yr
  - GHI: **2670** kWh/m<sup>2</sup>-yr
- Decision variable:
  - **PV Capacity**
  - **CSP Capacity**
  - **EZ Capacity**
- **H-B capacity** of 1,000 Ton/d
- KPI:
  - LCOE
  - LCOH
  - **LCOA**
  - **NH3 production**

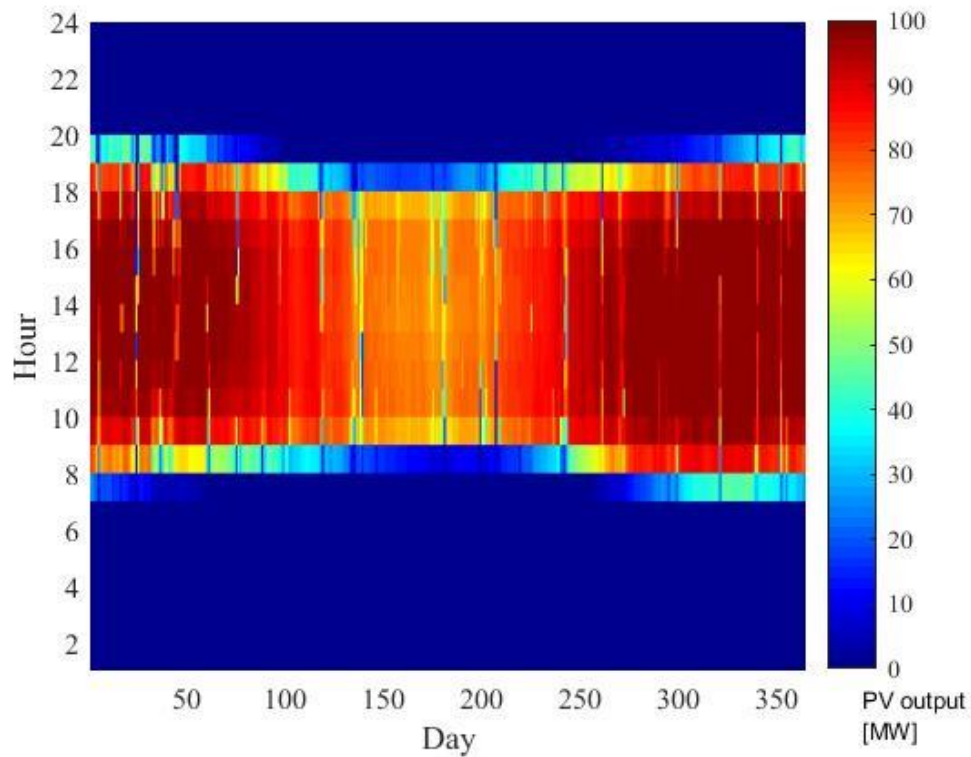


Capacity	Unit	Ref	Min	Max
PV	MW	800	500	1,500
CSP	MW	200	0	400
EZ	MW	600	500	1,500
H-B	Ton/d	1,000	-	-

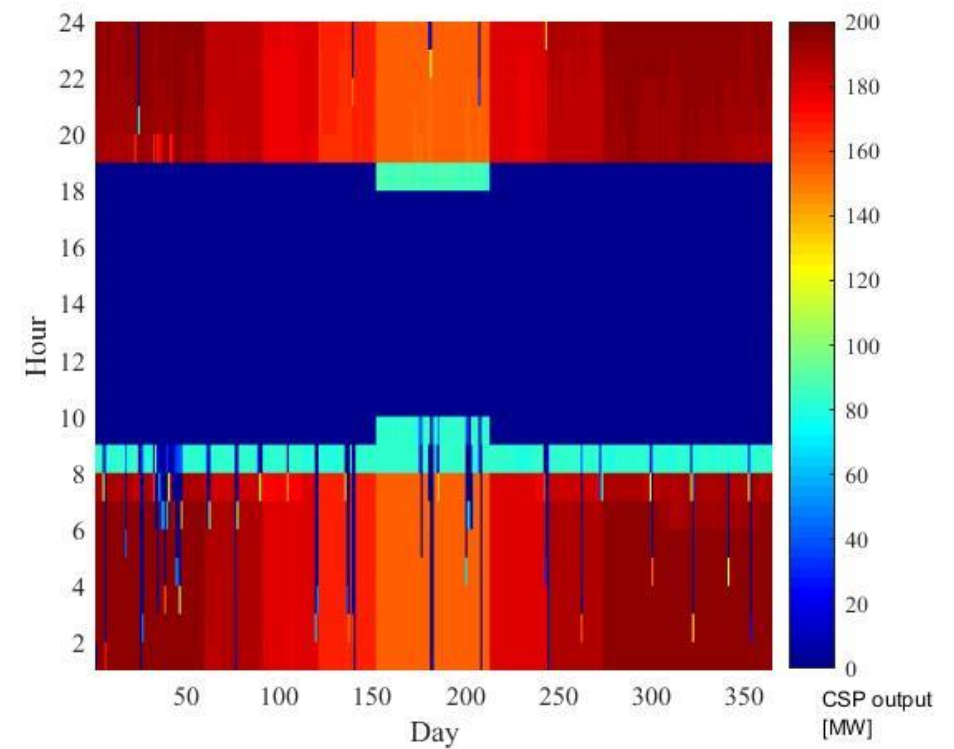


# Generation Plant – Power Profiles

- PV profile: full operation during the daylight hours.
- Main H2 production with PV.



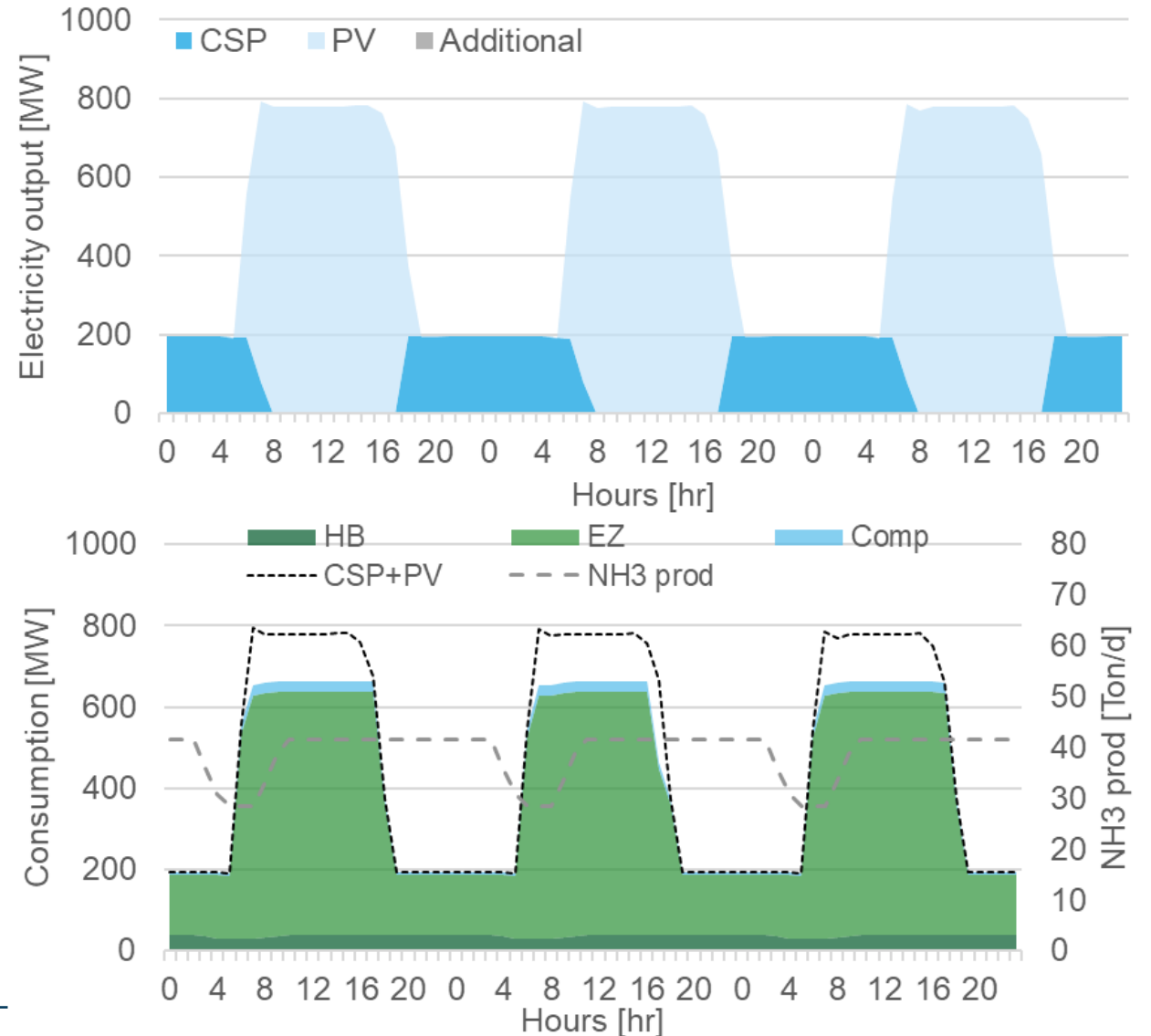
- CSP profile: focused on night operation.
- Optimize profile to deliver stable power considering a part-load operation.



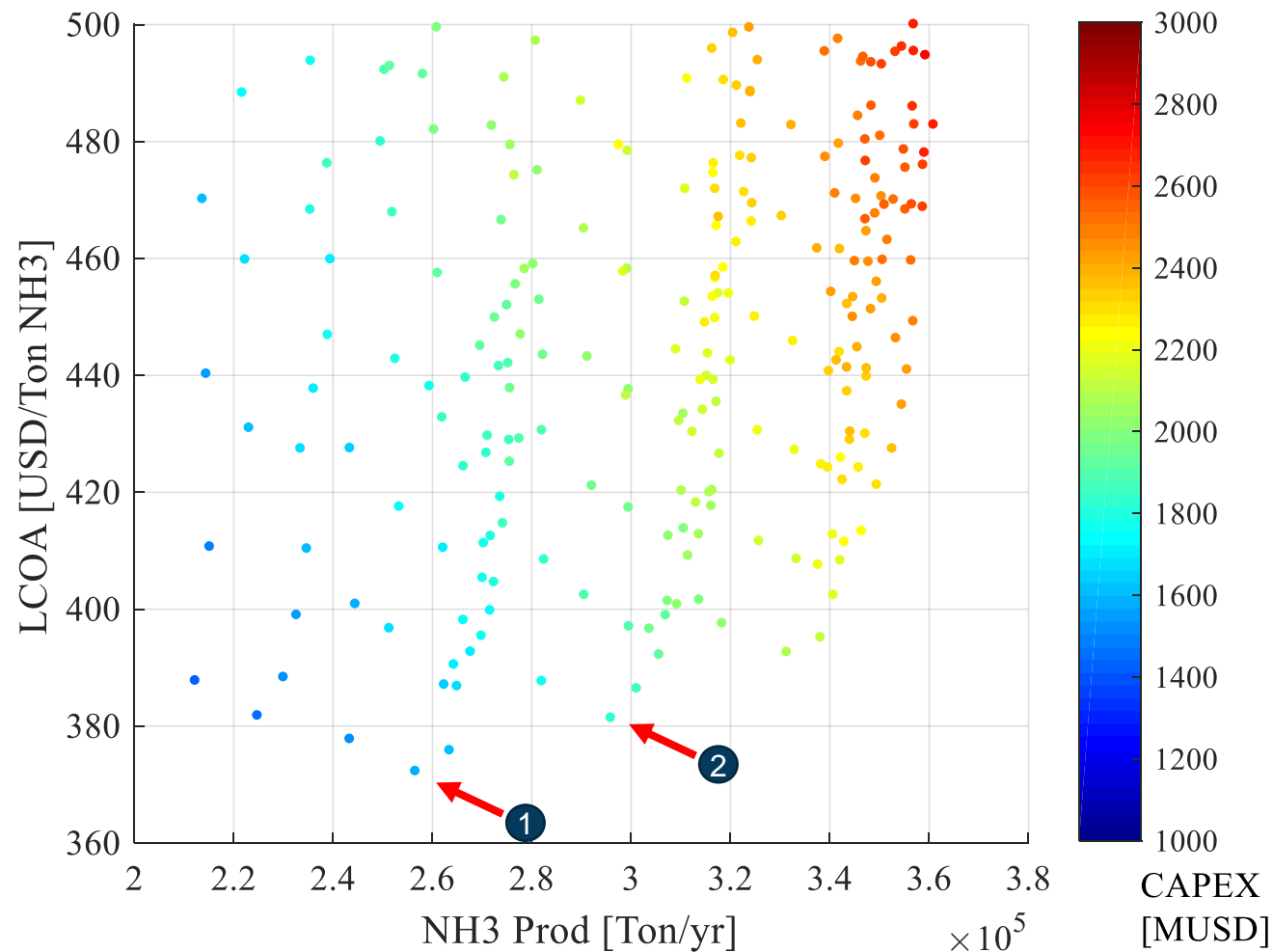


# Industrial Plant – Hourly Profile and Operation

- Electrolyzers operates in two modes:
  - Main **H2 production with PV** in daylight hours
  - CSP support** the H2 production during the night
- Hydrogen storage management** is key point.
- H-B operates** in terms of the H2 production and the available H2 stored.
  - Ramping and part-load operation.
  - Avoid shut-down.



# Results - Optimization



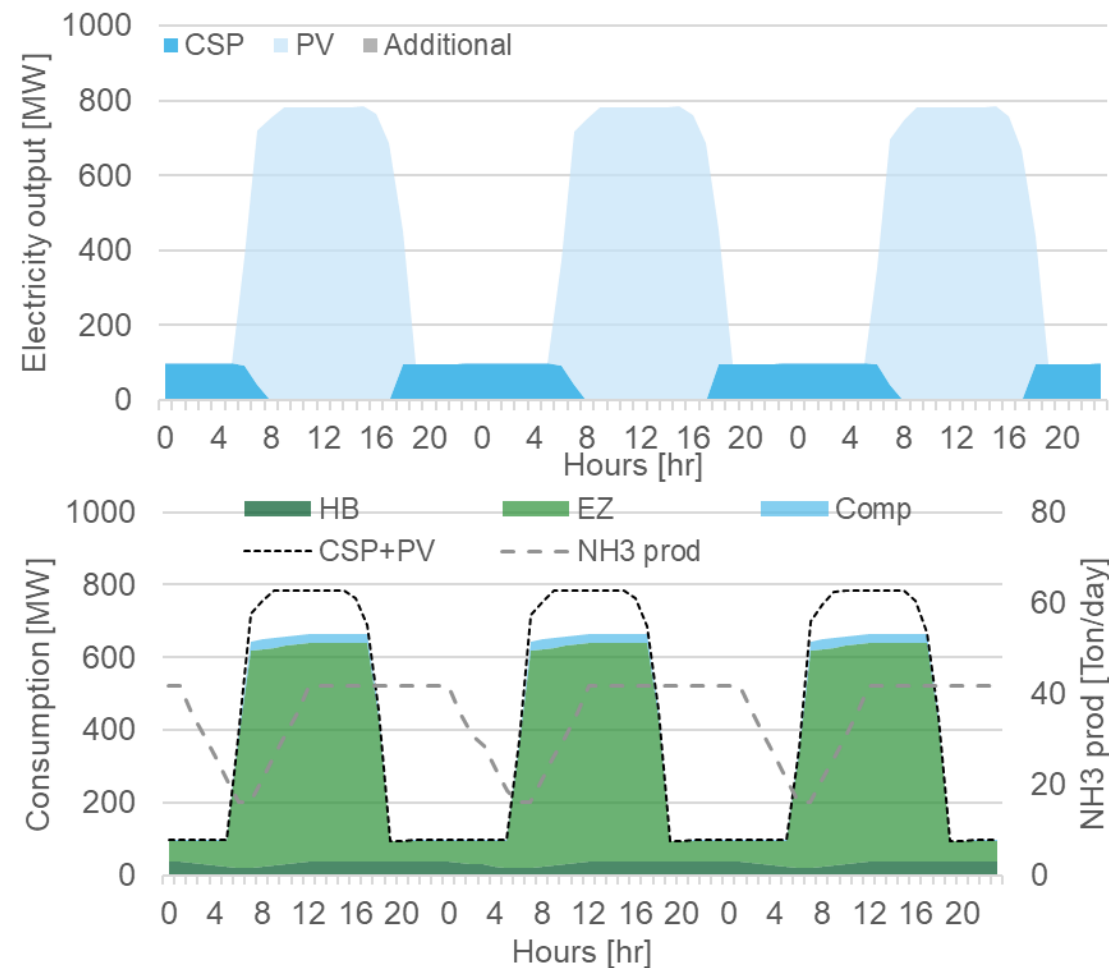
		Opt 1	Opt 2
CSP	MW	100	200
PV	MW	800	800
EZ	MW	600	600
HB	Ton/d	1,000	1,000
LCOE PV	USD/MWh	11.5	11.5
LCOE CSP	USD/MWh	41.9	41.5
LCOE (Combined)	USD/MWh	16.2	19.3
LCOH	USD/kg H <sub>2</sub>	1.53	1.62
LCOH (Stored)	USD/kg H <sub>2</sub>	1.77	1.84
LCOA	USD/Ton NH <sub>3</sub>	372.2	381.3
NH <sub>3</sub> production	NH <sub>3</sub> Ton/yr	257,451	296,924
H <sub>2</sub> production	H <sub>2</sub> Ton/yr	45,701	52,717
Total Generation	GWh	2,836	3270

2%

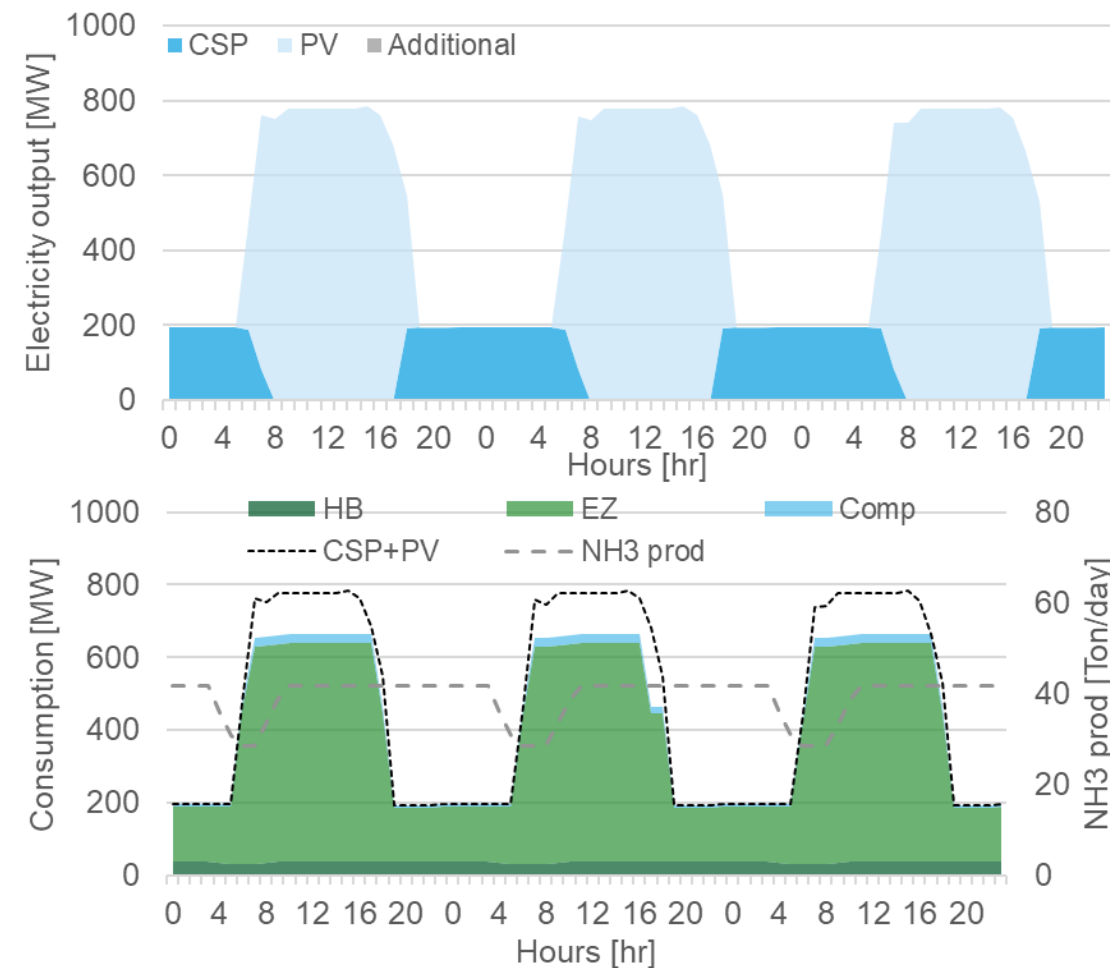
15%

# Results – Optimum profiles

Layout 1 case profile



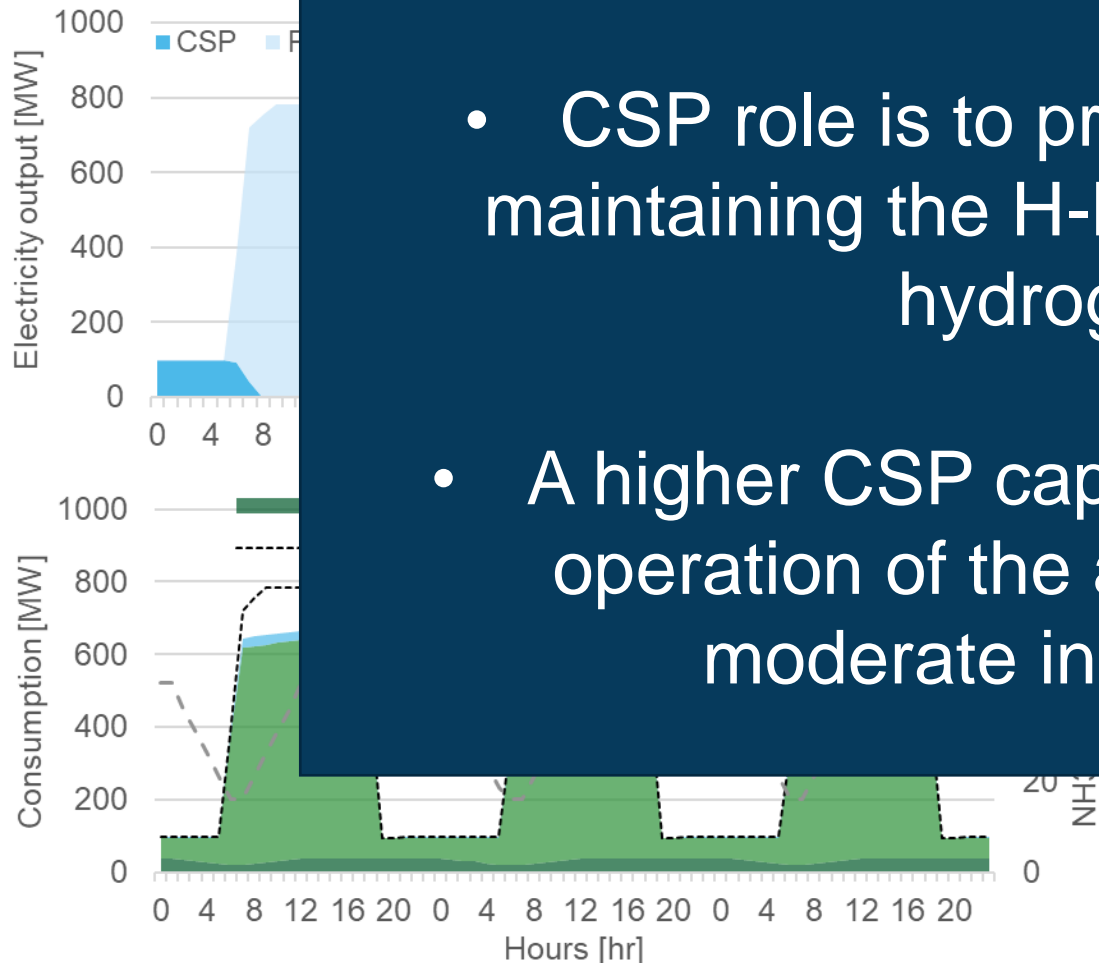
Layout 2 case profile



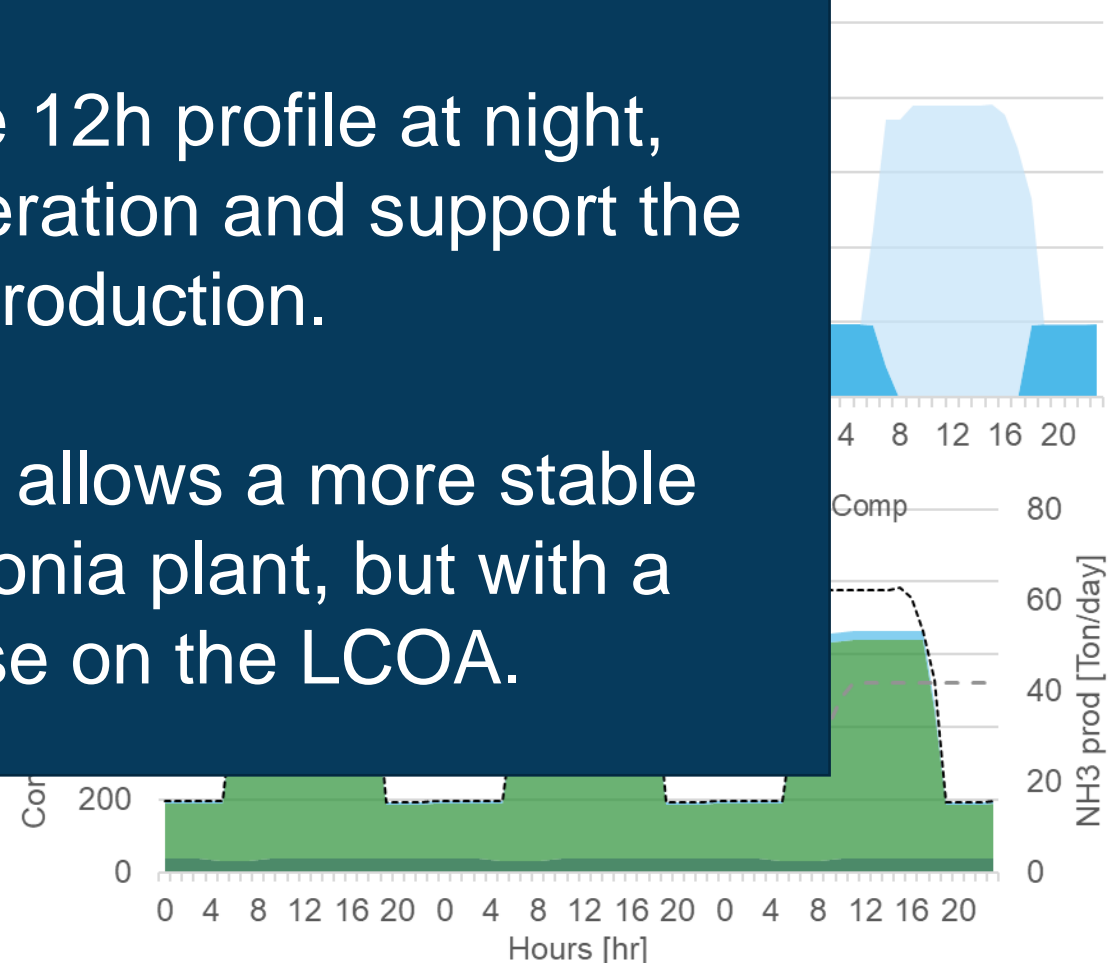


# Results – Optimum profiles

- Opt 1 case profile



- Opt 2 case profile

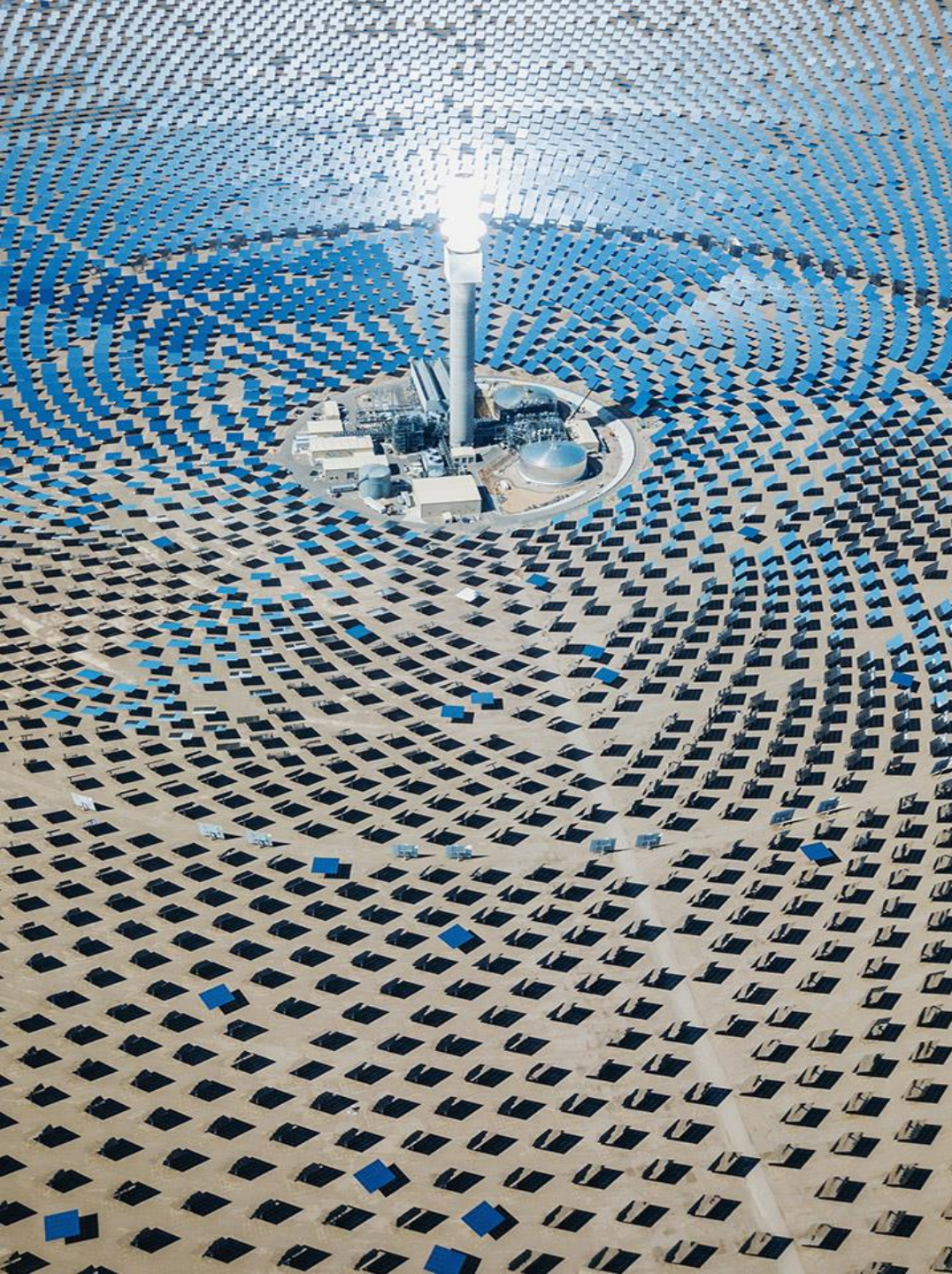


- CSP role is to provide 12h profile at night, maintaining the H-B operation and support the hydrogen production.
- A higher CSP capacity allows a more stable operation of the ammonia plant, but with a moderate increase on the LCOA.

# Conclusions

- CSP have an important role in the green hydrogen and ammonia industry.
- PV provide the low energy cost to produce  $H_2$ .
- The CSP design must provide stable power during 12h to the H-B reactor and complement the  $H_2$  production at night.
- The operational limitation of the H-B and  $H_2$  storage are crucial to define the limitation of the CSP+PV power profile.
- The CSP capacity is defined by the H-B capacity. A 1000 Ton/d H-B may require from 100 to 200 MW of CSP.





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