

How to reduce the LCoA of green NH₃ with hybrid CSP-PV plants

Xavier Lara, Carlos Mata-Torres

Pacific Green Solar Technologies, PGT Group.

xavier.lara@pacificgreen.tv

carlos.mata@pacificgreen.tv



PacificGreen
Solar Technologies



PacificGreen
Technologies Group

PGTK Technologies & Company Development

Leading environmental technologies group

Vision

PGTK's vision is a world in which the issues of climate heating and resource scarcity are addressed by technological innovation and sensible stewardship

Mission

PGTK's mission is to develop and deliver renewable technologies globally

Development

Evolved from a niche technologies development start-up into a globally recognized environmental and renewables group across multiple sectors



Rapid five-year development across seven different technologies



Marine FGD Systems



Land-Based FGD Systems



Photovoltaic Solar



Concentrated Solar Power



Freshwater Desalination



Battery Energy Storage Systems



Hydrogen Production

2016

2017

2018

2019

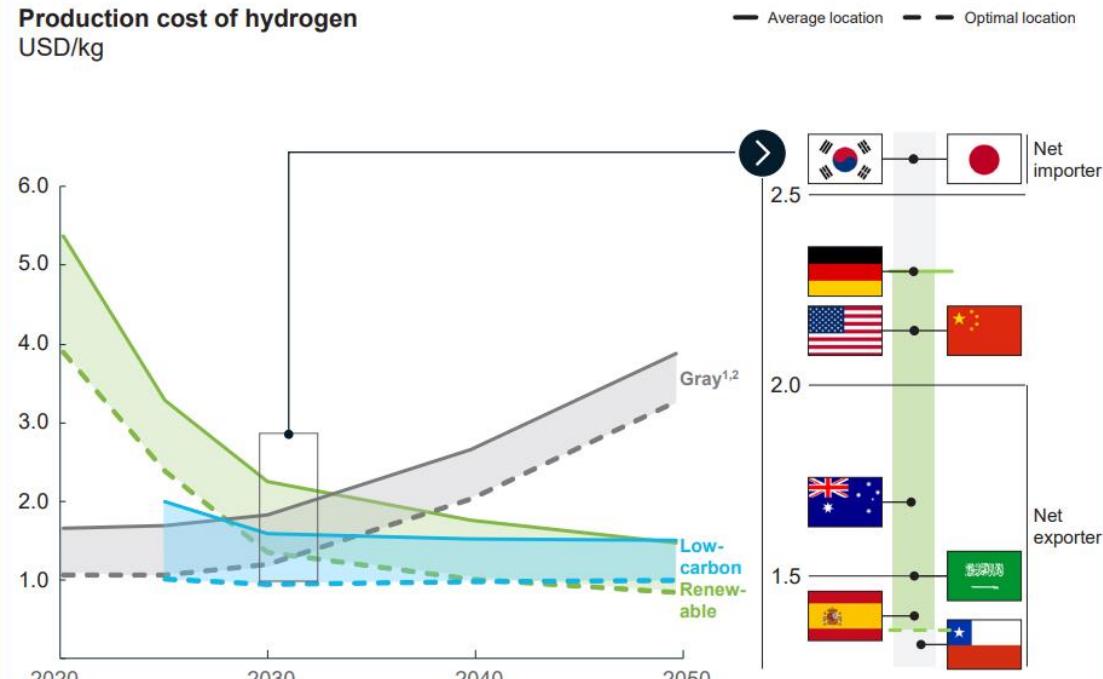
2020

2021

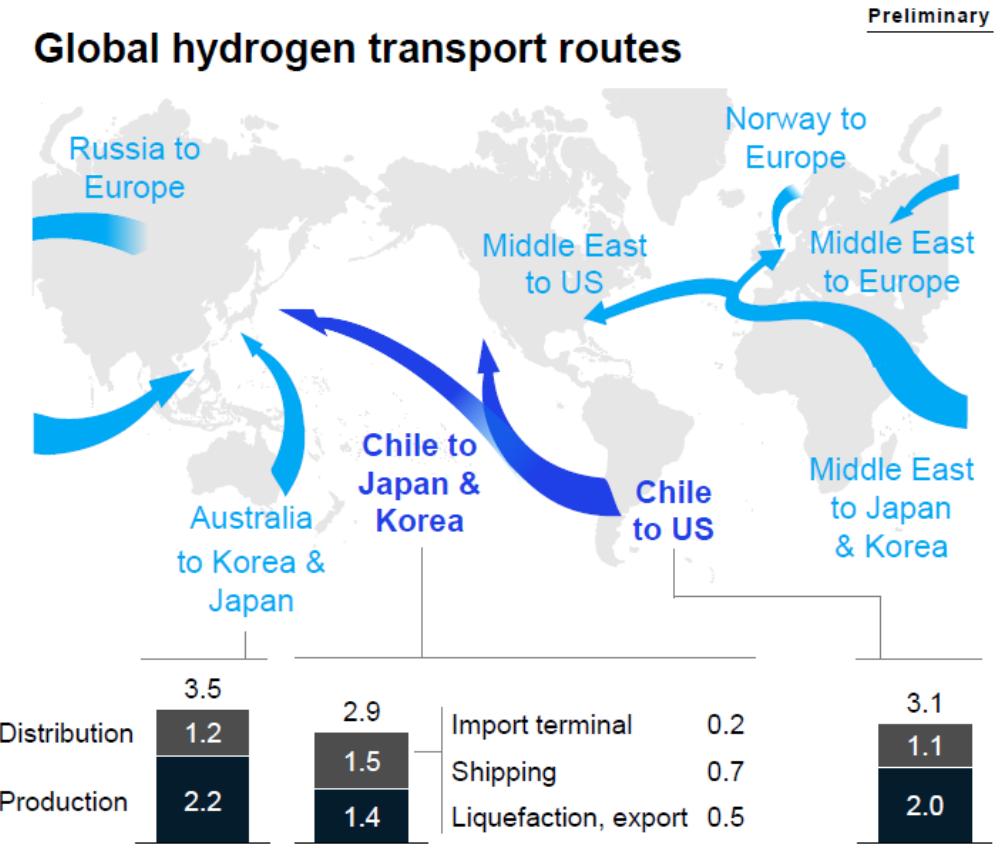
Context – Huge hype for Green Hydrogen

Exhibit 7: Hydrogen production pathways, including carbon costs

Production cost of hydrogen
USD/kg



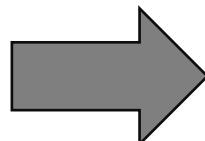
Global hydrogen transport routes



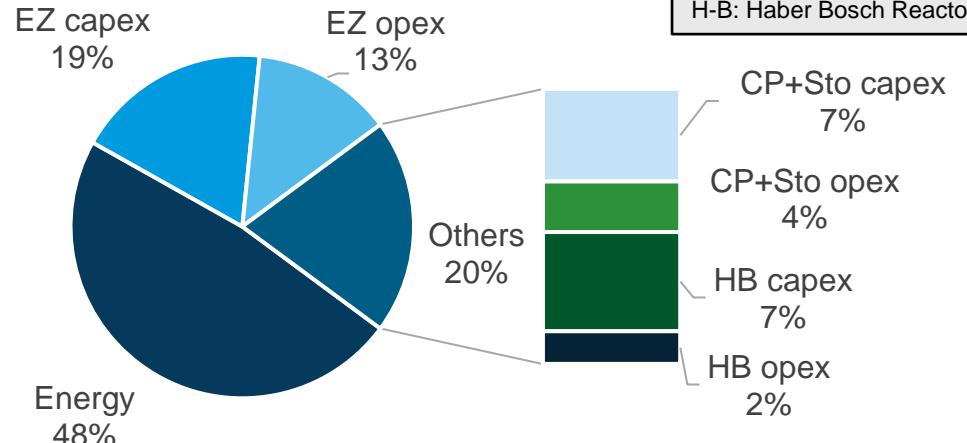
Context – From Green Hydrogen to Green Ammonia

- Ammonia production is mainly made by a Haber-Bosch Reactor
- Ammonia is one of the most demanded chemical in the industry
- It has the potential to be used as an energy carrier of the Hydrogen

How to make the H_2 and NH_3 Green with Solar?

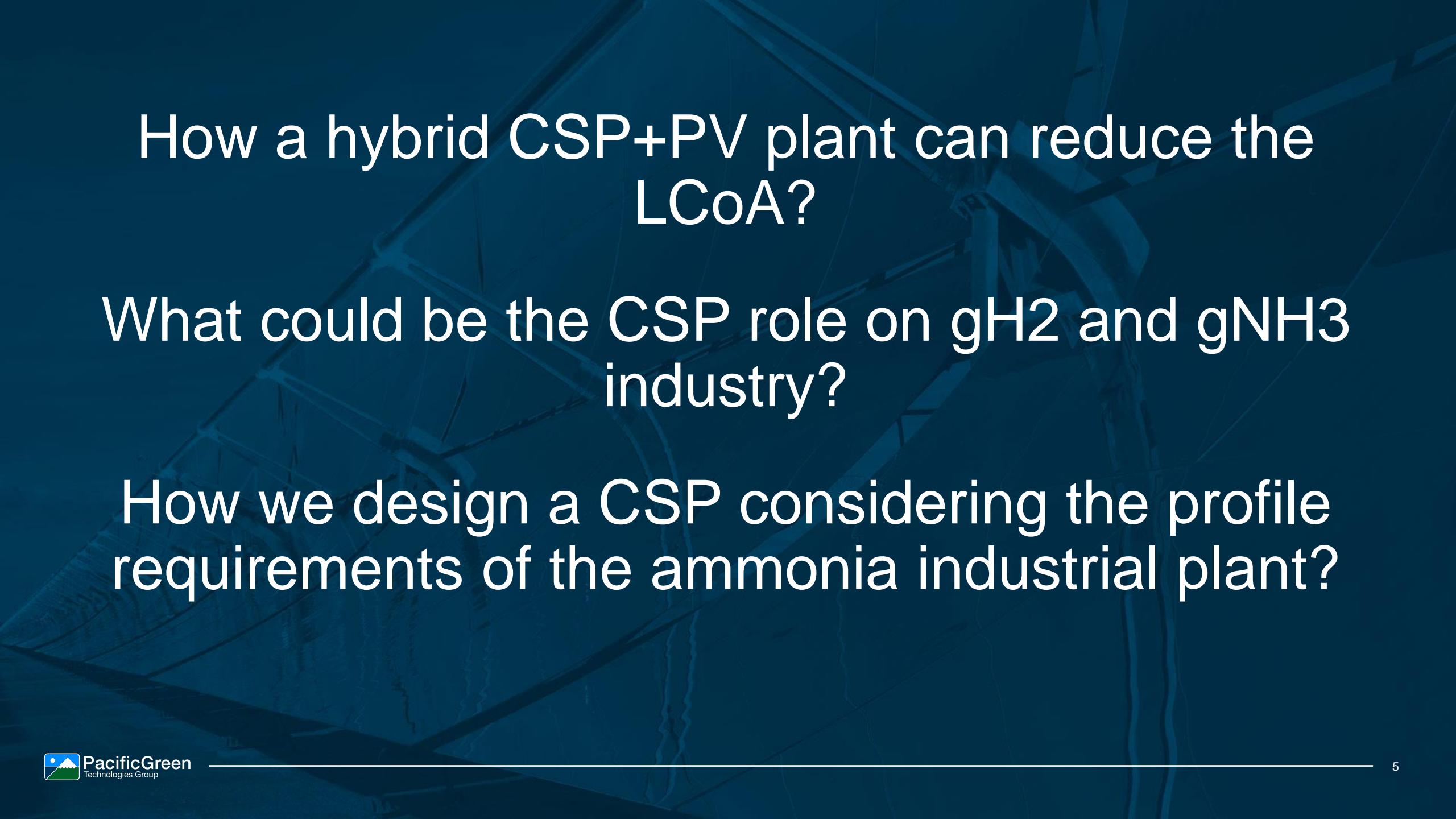


Breakdown of gNH₃ cost



Energy cost is the most relevant factor

The best option is
PV+CSP technology.

A dark blue background image showing a close-up perspective of a solar panel array, with the panels forming a grid pattern.

How a hybrid CSP+PV plant can reduce the LCoA?

What could be the CSP role on gH₂ and gNH₃ industry?

How we design a CSP considering the profile requirements of the ammonia industrial plant?

System Description – CSP+PV Generation Plant and H₂+NH₃ Industrial Plant

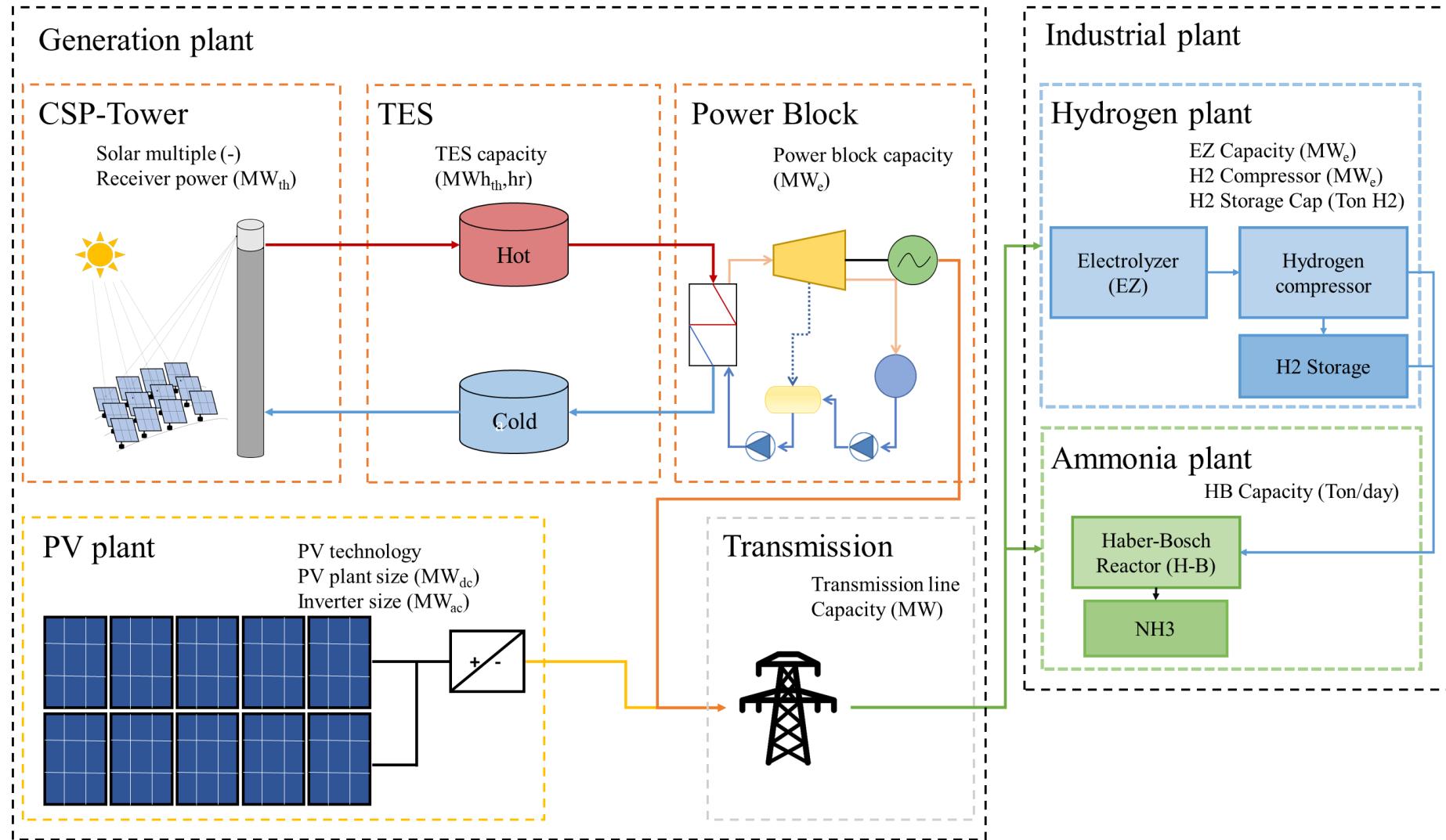
Main system

Generation plant:

- CSP Tower [MW]
- PV plant [MW]

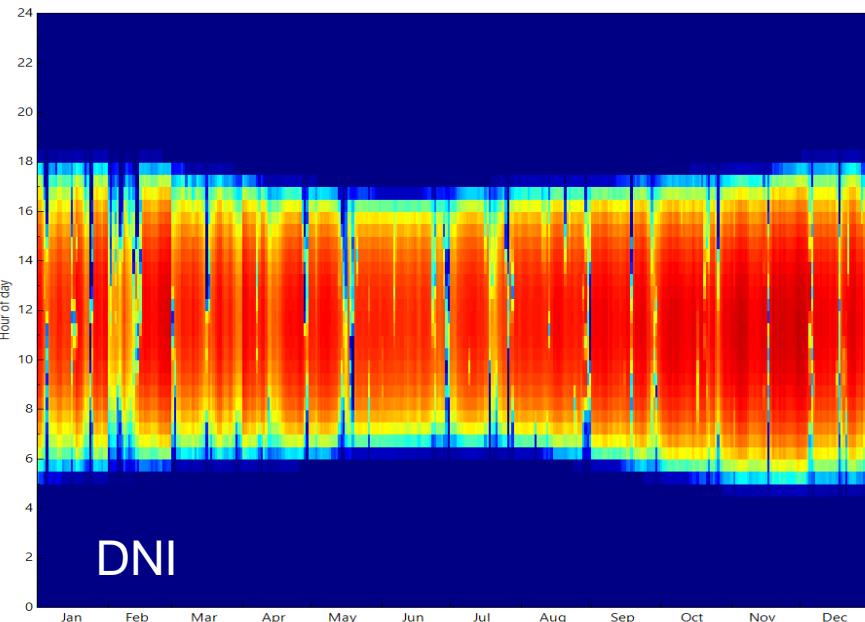
Industrial plant

- Electrolyzer [MW]
- H₂ Compressor [MW]
- H₂ Storage [Ton]
- Haber-Bosch Reactor [Ton/d]

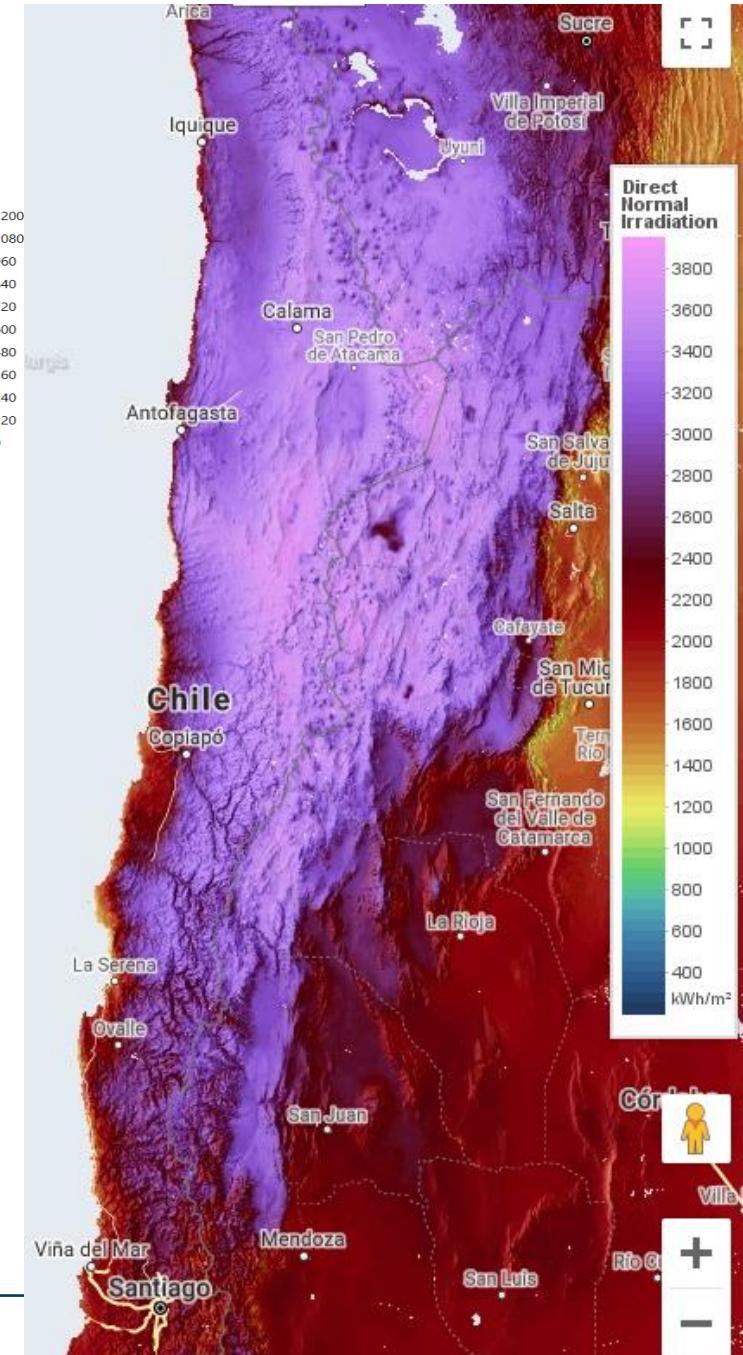


Case of Study – Chile Atacama Desert

- Analysis performed for northern Chile - Atacama Desert conditions.
 - DNI: **3500 kWh/m²-yr**
 - GHI: **2670 kWh/m²-yr**
- Decision variable:
 - **PV Capacity**
 - **CSP Capacity**
 - **EZ Capacity**
- **H-B capacity** of 1,000 Ton/d
- KPI:
 - LCOE
 - LCOH
 - LCOA
 - **NH₃ production**

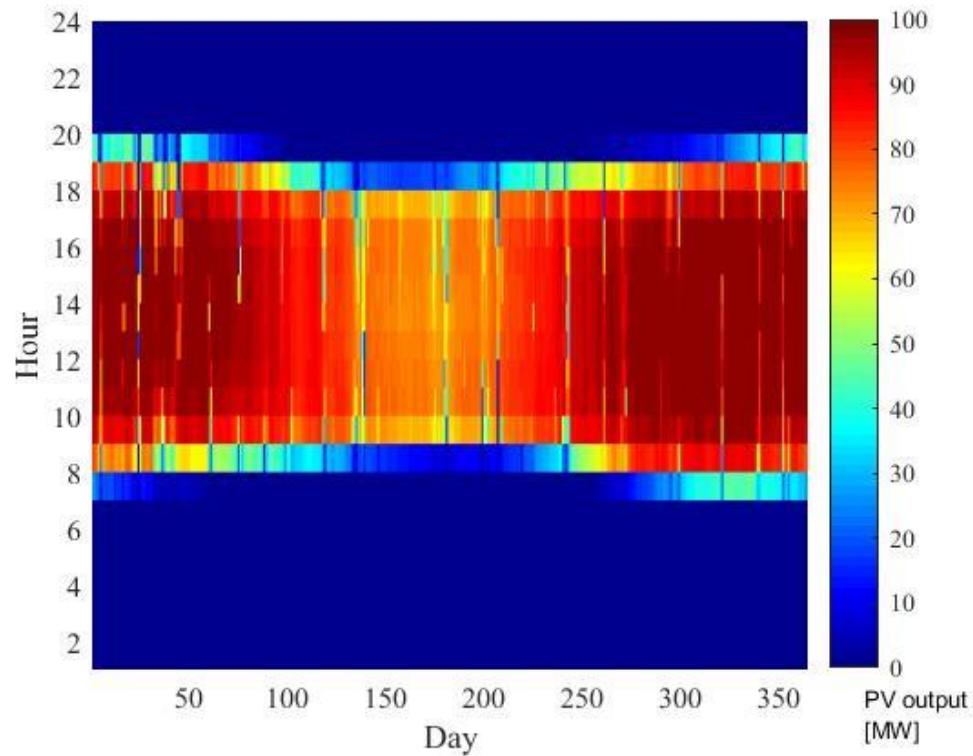


| Capacity | Unit | Ref | Min | Max |
|----------|-------|-------|-----|-------|
| PV | MW | 800 | 500 | 1,500 |
| CSP | MW | 200 | 0 | 400 |
| EZ | MW | 600 | 500 | 1,500 |
| H-B | Ton/d | 1,000 | - | - |

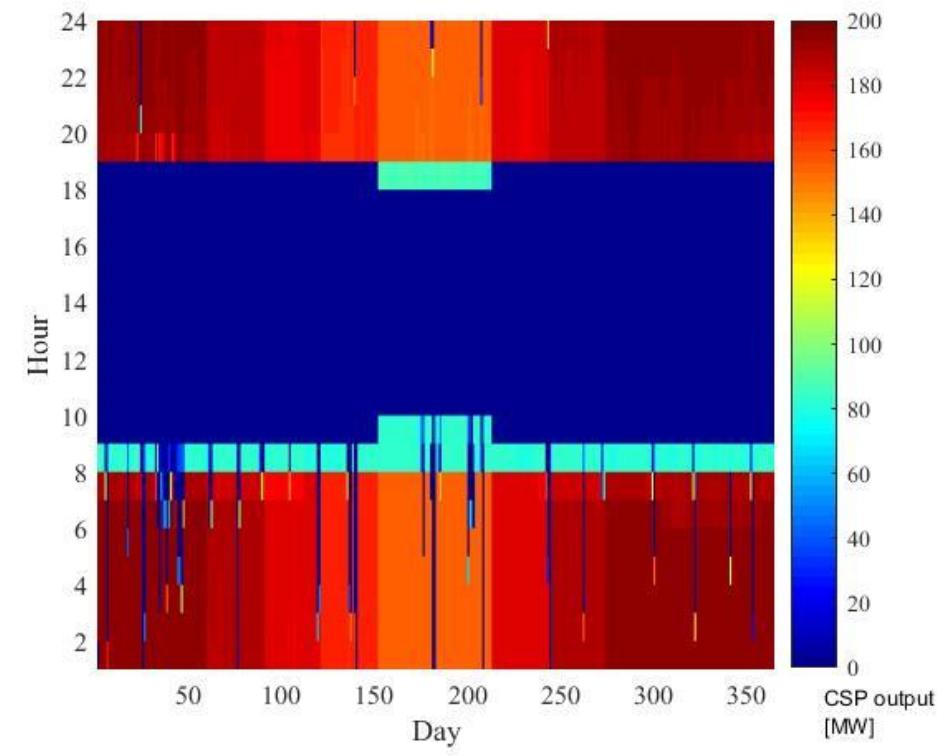


Generation Plant – Power Profiles

- PV profile: full operation during the daylight hours.
- Main H₂ production with PV.

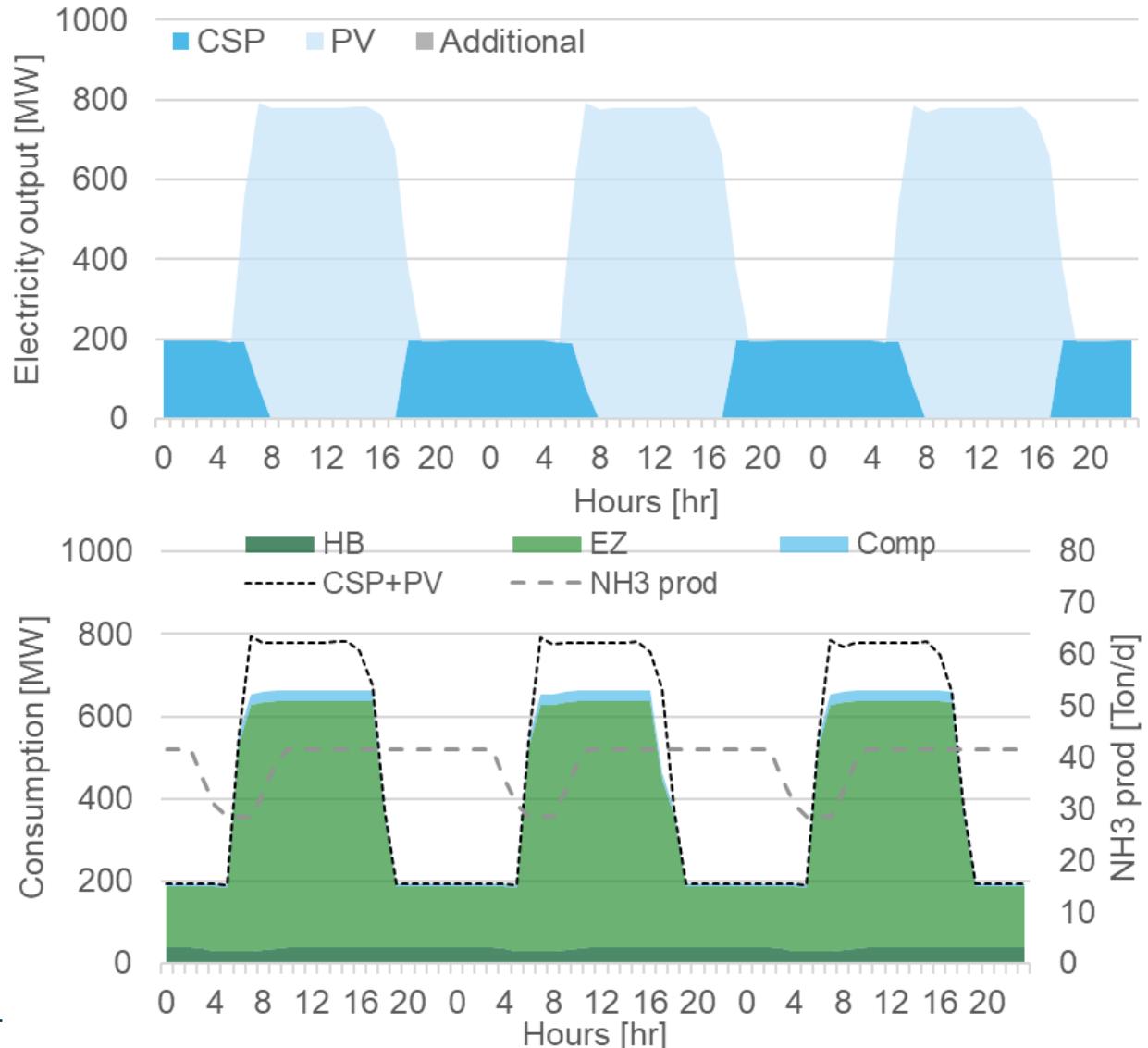


- CSP profile: focused on night operation.
- Optimize profile to deliver stable power considering a part-load operation.

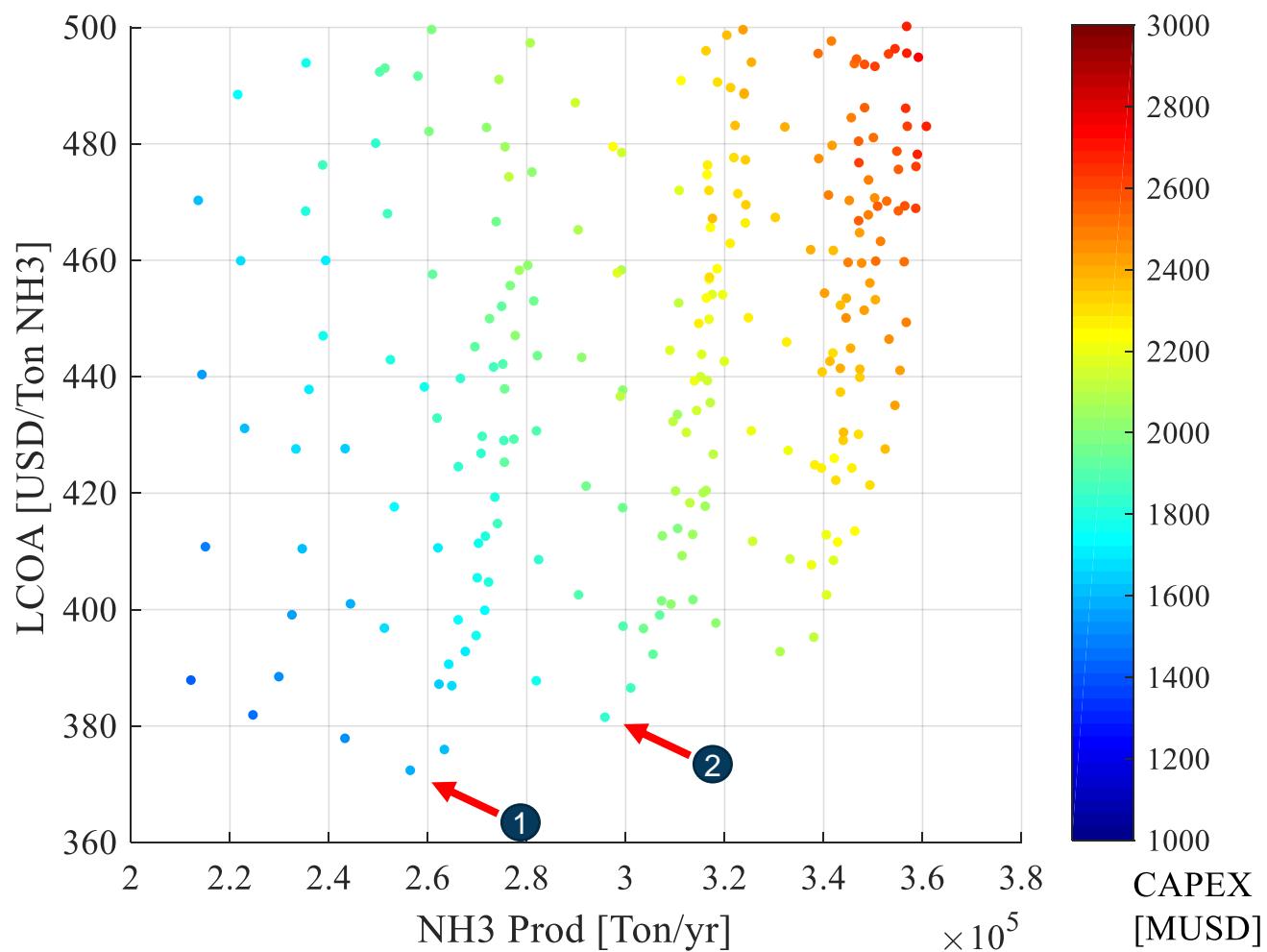


Industrial Plant – Hourly Profile and Operation

- Electrolyzers operates in two modes:
 - Main **H2 production with PV** in daylight hours
 - **CSP support** the H2 production during the night
- **Hydrogen storage management** is key point.
- **H-B operates** in terms of the H2 production and the available H2 stored.
- Critical H-B operation limitation
 - Ramping and part-load operation.
 - Avoid shut-down.



Results - Optimization

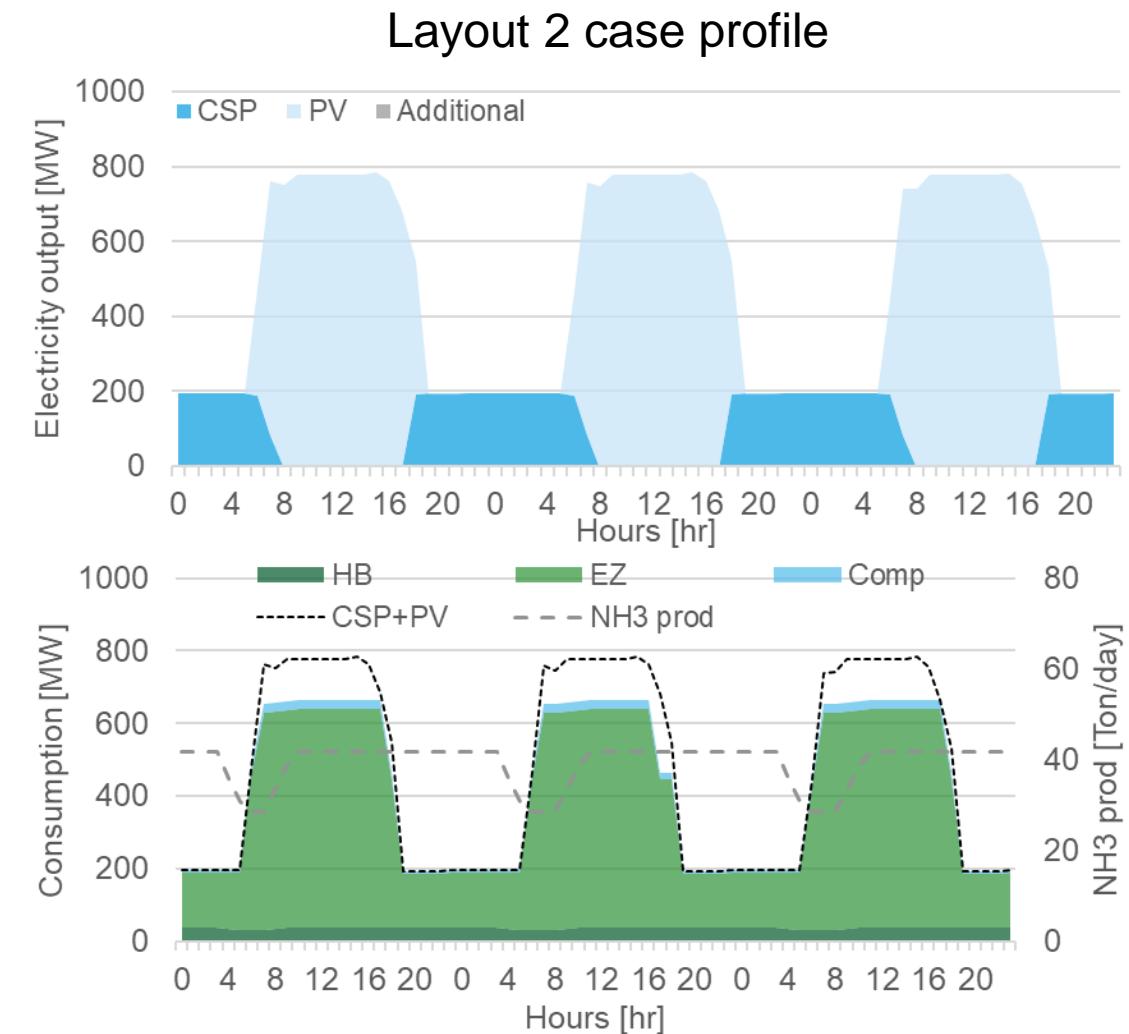
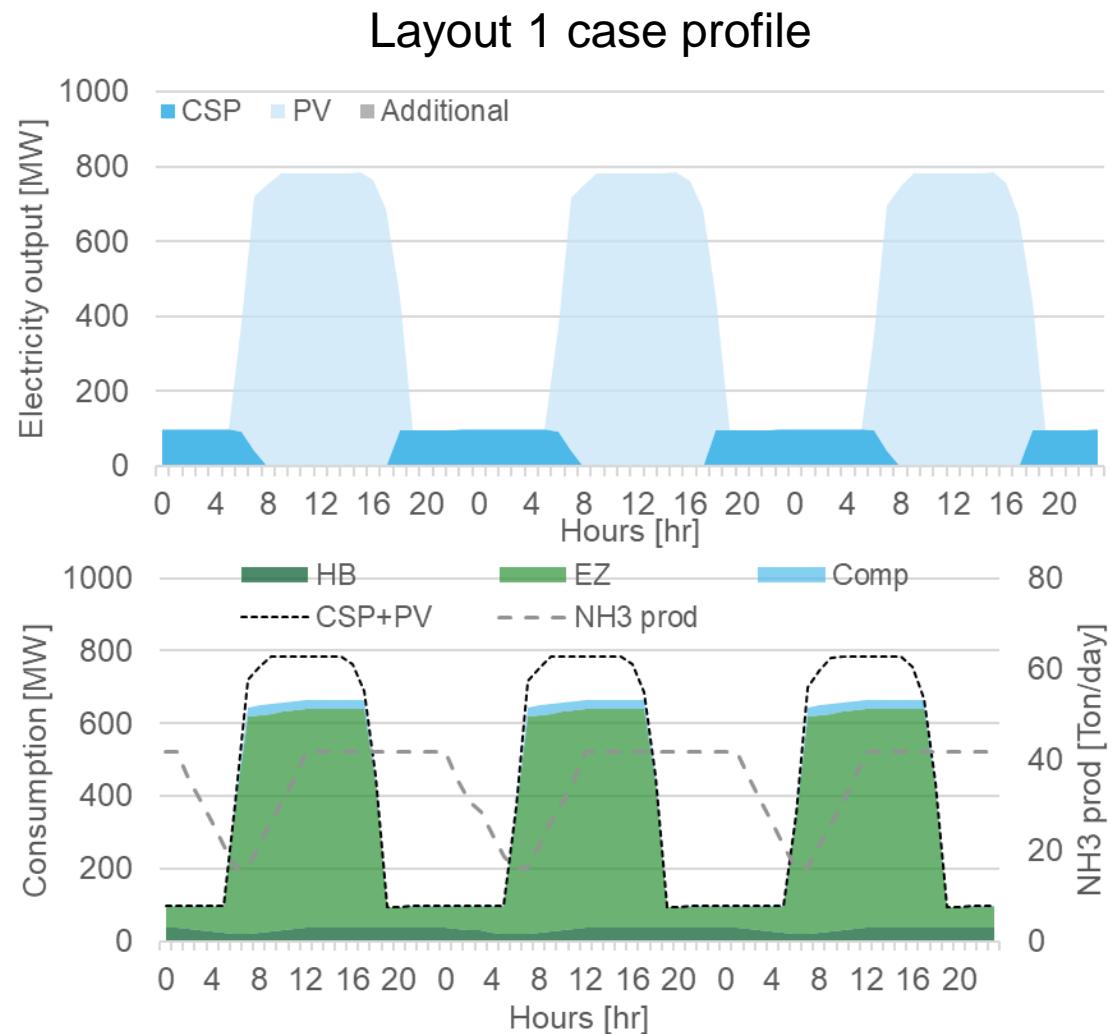


| | | Opt 1 | Opt 2 |
|----------------------------|-------------------------|---------|---------|
| CSP | MW | 100 | 200 |
| PV | MW | 800 | 800 |
| EZ | MW | 600 | 600 |
| HB | Ton/d | 1,000 | 1,000 |
| LCOE PV | USD/MWh | 11.5 | 11.5 |
| LCOE CSP | USD/MWh | 41.9 | 41.5 |
| LCOE (Combined) | USD/MWh | 16.2 | 19.3 |
| LCOH | USD/kg H ₂ | 1.53 | 1.62 |
| LCOH (Stored) | USD/kg H ₂ | 1.77 | 1.84 |
| LCOA | USD/Ton NH ₃ | 372.2 | 381.3 |
| NH ₃ production | NH ₃ Ton/yr | 257,451 | 296,924 |
| H ₂ production | H ₂ Ton/yr | 45,701 | 52,717 |
| Total Generation | GWh | 2,836 | 3,270 |

2%

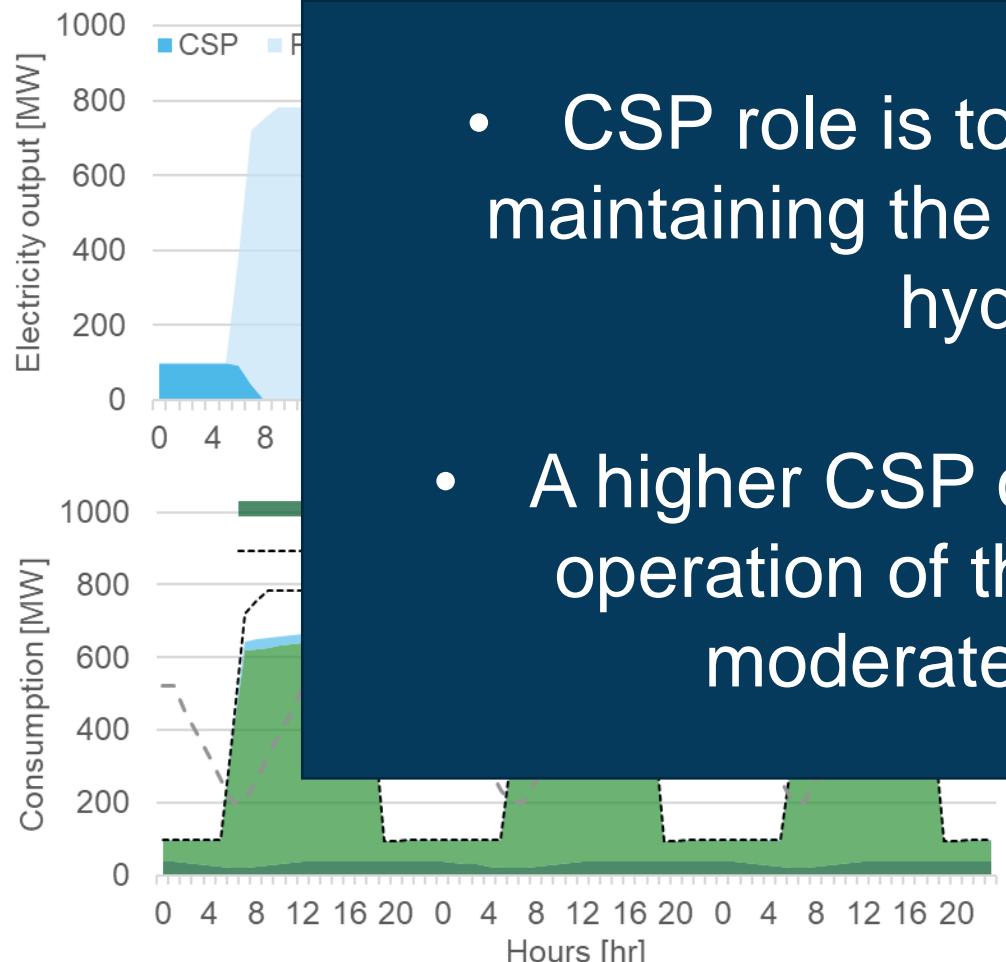
15%

Results – Optimum profiles



Results – Optimum profiles

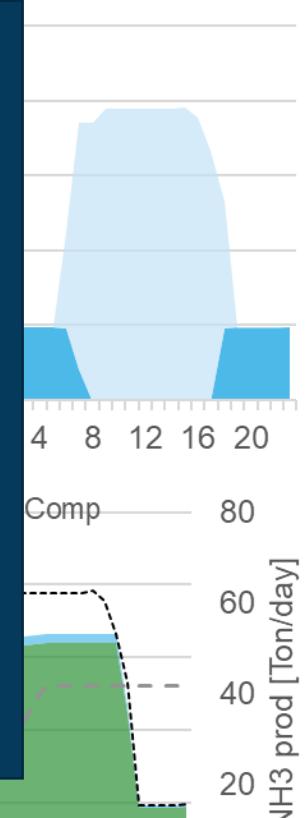
- Opt 1 case profile



- Opt 2 case profile

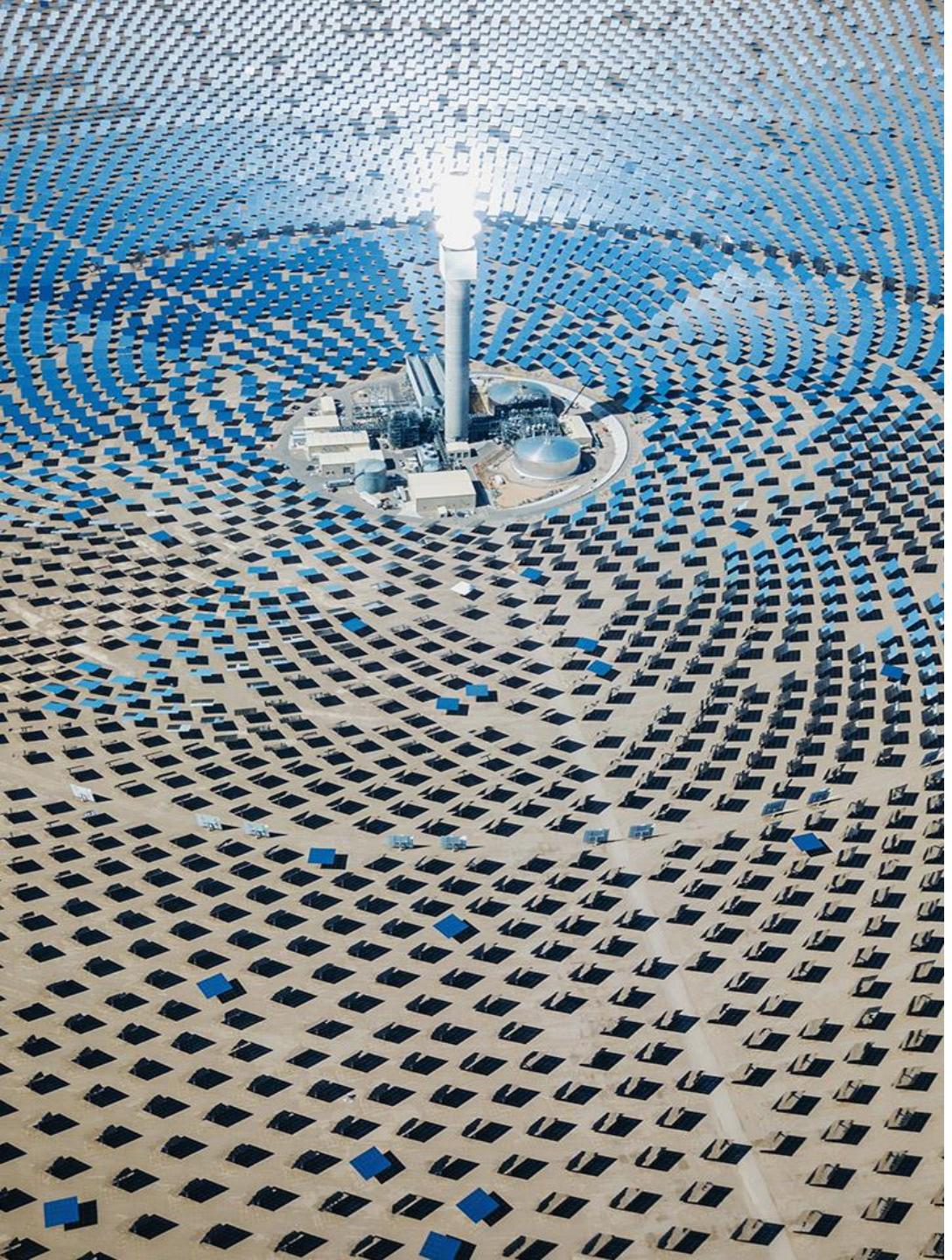
• CSP role is to provide 12h profile at night, maintaining the H-B operation and support the hydrogen production.

• A higher CSP capacity allows a more stable operation of the ammonia plant, but with a moderate increase on the LCOA.



Conclusions

- CSP have an important role in the green hydrogen and ammonia industry.
- PV provide the low energy cost to produce H₂.
- The CSP design must provide stable power during 12h to the H-B reactor and complement the H₂ production at night.
- The operational limitation of the H-B and H₂ storage are crucial to define the limitation of the CSP+PV power profile.
- The CSP capacity is defined by the H-B capacity. A 1000 Ton/d H-B may require from 100 to 200 MW of CSP.



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