

Wednesday, October 31  
AIChE Annual Meeting 2018  
NH<sub>3</sub> Energy+  
549g

## **Evaluation of the cement clinker fired in the combustion furnace of heavy-oil and NH<sub>3</sub>**

○Hiroki Kujiraoka<sup>1</sup>, Tatsurou Izumi<sup>1</sup>, Yuya Yoshizuru<sup>1</sup>,  
Takeshi Suemasu<sup>1</sup>, Makoto Ueda<sup>1</sup>, Toyoaki Niki<sup>1</sup>, Takayasu Itou<sup>1</sup>,  
Masayuki Nishio<sup>1</sup>, Ryuichi Murai<sup>2</sup> and Fumiteru Akamatsu<sup>2</sup>  
(1) UBE Industries, LTD. (2) Osaka University

- Business Overview on UBE Industries, LTD
- Background
- Toward Applying  $\text{NH}_3$  energy for Cement process
  - ✓ Burning cement clinker in exhaust-gas atmosphere (Ex.1)
  - ✓ Evaluation of clinker fired by  $\text{NH}_3$  and heavy-oil (Ex.2)
- Conclusion

# Business Overview on UBE Industries, LTD.

➤ FY2017 Consolidated Net Sales: ¥695.5 billion

**Chemicals**  
44% of net sales  
¥305.4 billion ※



- Nylon raw materials and resin
- Synthetic rubber
- Industrial chemicals
- Specialty products
- Battery materials
- Fine chemicals

**Pharmaceuticals**  
1% of net sales  
¥10.2billion



- Drug discovery and co-development
- Contract manufacturing

**Cement & Construction Materials**  
34% of net sales, ¥238.8billion



- Cement, ready-mixed concrete
- Building materials
- Calcia, magnesia

**Machinery**  
13% of net sales  
¥90.1 billion



- Molding machines (Injection molding machines, die-casting machines)
- Industrial machinery
- Bridge

**Energy & Environment**  
10% of net sales  
¥71.3 billion



- Coal storage/sales
- IPP/Power business

※: Inter-segment internal sales are included (percentages add up to above 100%).

➤ We have **ammonia (NH<sub>3</sub>)** and **cement** manufacturing process

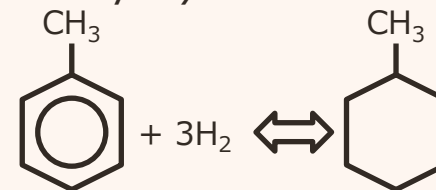
## SIP “Energy Career”

Metal Hydride

Liquefied H<sub>2</sub>  
-253 °C

Ammonia (NH<sub>3</sub>)  
**Direct combustion**

Methyl cyclo-hexane



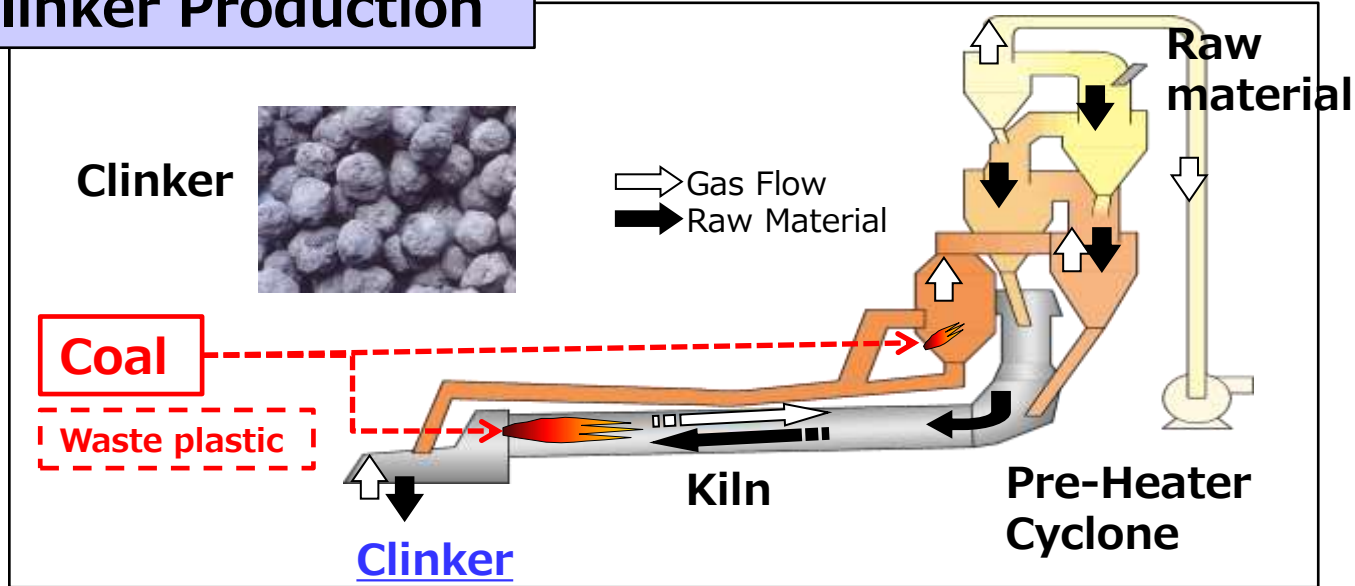
Cross-ministerial Strategic Innovation Promotion Program (SIP) “Energy Career”  
by Council for Science, Technology and Innovation (CSTI) in Japan

We’ve been participating in SIP “Energy Career” since 2014,  
**toward applying NH<sub>3</sub> energy for industrial furnace (cement kiln)**

1. Burned clinker in electric furnace of exhaust-gas atmosphere
2. Fired NH<sub>3</sub> energy in test furnace
3. Fired clinker by NH<sub>3</sub> energy in test furnace
4. Process simulation and CFD for our commercial plant

# 【Background】 Cement Manufacturing Process

## Clinker Production



- ✓ **Clinker** ;  $\text{CaCO}_3$ , Silica, Clay and Fe Source mixtures burned at  $1450\text{ }^\circ\text{C}$
- ✓ **Cement** ; mixture of clinker and  $\text{CaSO}_4 \cdot 2\text{H}_2\text{O}$  (di-hydrated gypsum)

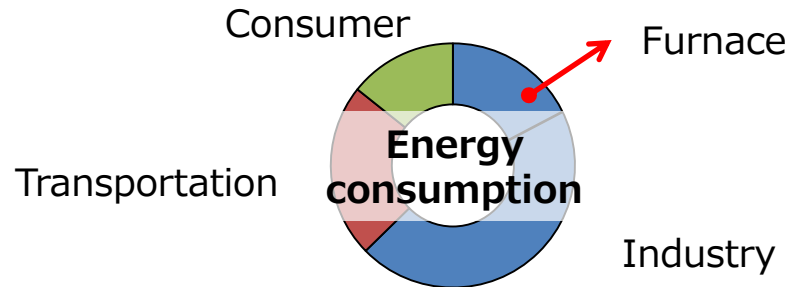
➤ **Mixed  $\text{NH}_3$  Combustion would be reduce  $\text{CO}_2$  Emission**

# 【Background】 Estimation CO<sub>2</sub> reduction in cement

Industrial furnace account for

**17%** Energy consumption in Japan

Agency for Natural Resources and Energy (2016),  
 “Japan’s Energy White Paper”, September



## Estimation CO<sub>2</sub> reduction effect

Based on average coal usage in cement process, estimate CO<sub>2</sub> reduction effect by replacing NH<sub>3</sub>

※Following values were used for estimation  
 【Heat value】 Coal : 25.95, NH<sub>3</sub> : 18.8 MJ/kg  
 【Coal comp.】 C:65, H:4, O:4, N:2, Ash:25 wt%

	Average ('11-'15) (1K ton/year)
Clinker production	50,319
Coal usage	6,680
Total energy consumption	8,967

Cement Handbook, Japan Cement Association (2016)

Replaced NH <sub>3</sub> (cal. %)	NH <sub>3</sub> requirement (1K ton/year)	Coal usage (1K ton/year)	CO <sub>2</sub> emission (1K ton/year)	CO <sub>2</sub> reduction (1K ton/year)
0	0	6680	15,921	0
1	92	6613	15,761	159

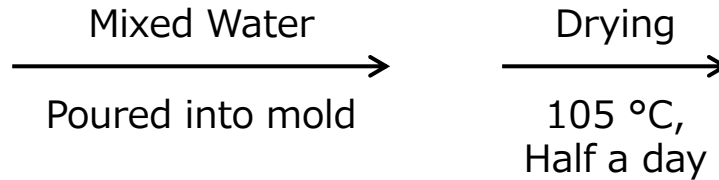
➤ Replacing 1% Coal with NH<sub>3</sub> could reduce 160 kton-CO<sub>2</sub>/year

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# [Experiment] Materials

## □ Materials for clinker

- ◆ Calcium carbonate
- ◆ Silica stone powder
- ◆ Fly ash (JIS II)
- ◆ Reagent  
( $Fe_2O_3$ ,  $Na_2CO_3$ ,  
 $K_2CO_3$ ,  $CaSO_4 \cdot 2H_2O$ )



□ 10mm pellets



## □ Clinker modules for mixing ratio of raw materials

	Ex.1	Ex.2
H.M.	2.10	2.10
S.M.	2.45	2.77
I.M.	1.80	1.57

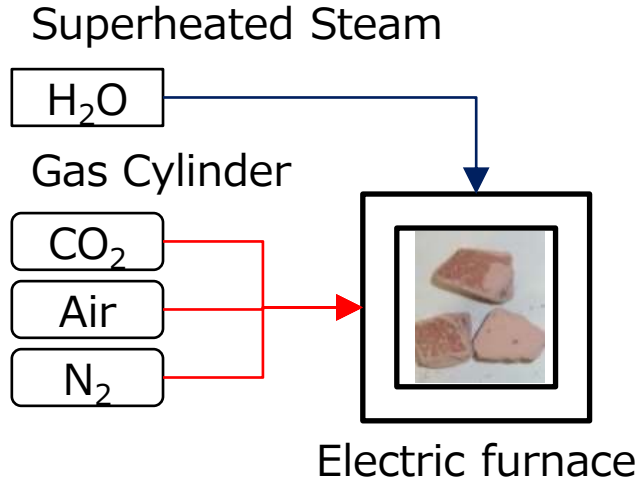
$$H.M. = \frac{CaO - (0.7SO_3)}{SiO_2 + Al_2O_3 + Fe_2O_3}$$

$$S.M. = \frac{SiO_2}{Al_2O_3 + Fe_2O_3}$$

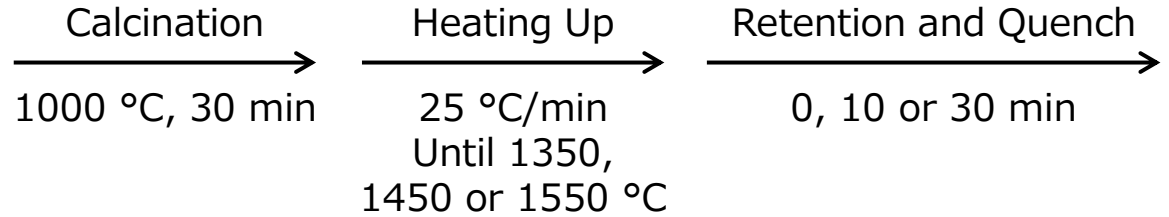
$$I.M. = \frac{Al_2O_3}{Fe_2O_3}$$

# [Experiment 1] Burning clinker in electric furnace

## □ Procedure



Combustion Conditions	Gas Conditions (Vol.%)			
	CO <sub>2</sub>	H <sub>2</sub> O	N <sub>2</sub>	O <sub>2</sub>
Coal	16.4	6.3	73.4	3.9
30%NH <sub>3</sub> Mixed	10.7	14.6	71.1	3.6



□ Analysis Minerals (XRD/Rietveld), free-CaO (JCAS-01(1997))

□ Calculation of reaction rate (Jander equation)

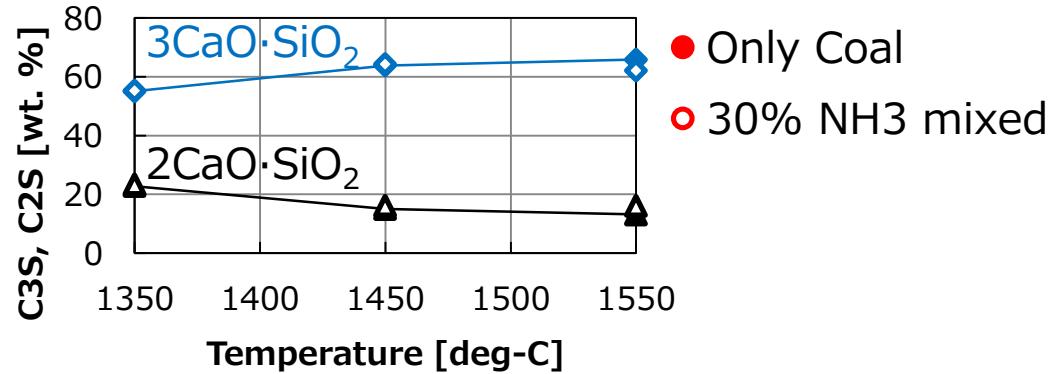
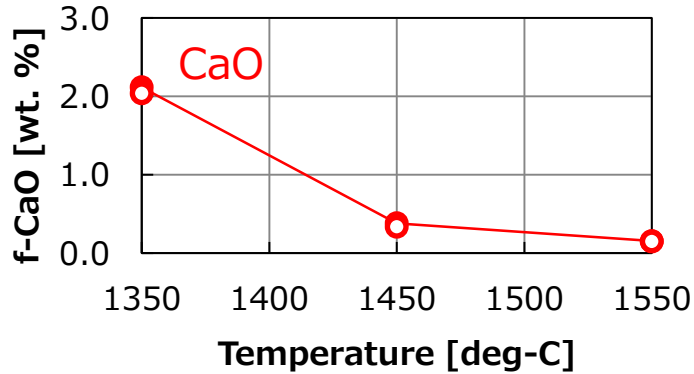
$$(1 - \sqrt[3]{1 - \alpha})^2 = A \exp\left(\frac{-E}{RT}\right) t$$

W. Jander, *Z Anorg Allg. Chem.*, 163, 1 (1927)

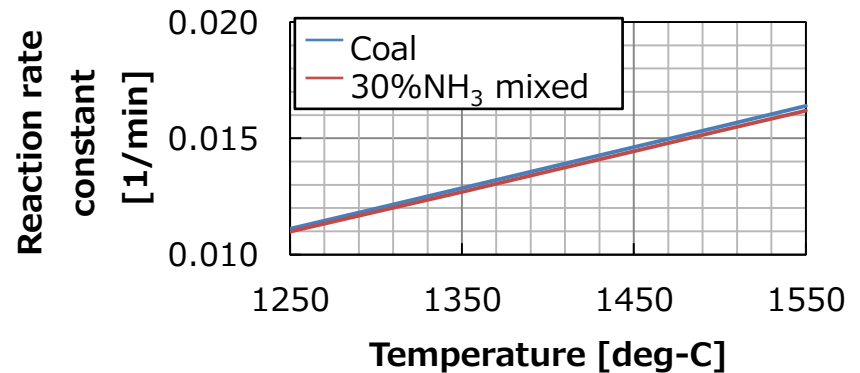
Defined  $E=29.92$  kJ/mol **Calculated A**

[Nomenclature]  $\alpha$ : Free-CaO reaction rate (-),  $A$ : Frequency factor (1/min),  $T$ : Temperature (K),  $E$ : Activation energy (J/mol),  $R$ : Gas constant (8.314 J/(mol K)),  $t$ : Retention time (min)

# [Results] Minerals and reaction rate in clinker



Sample picture (retention time: 10min)



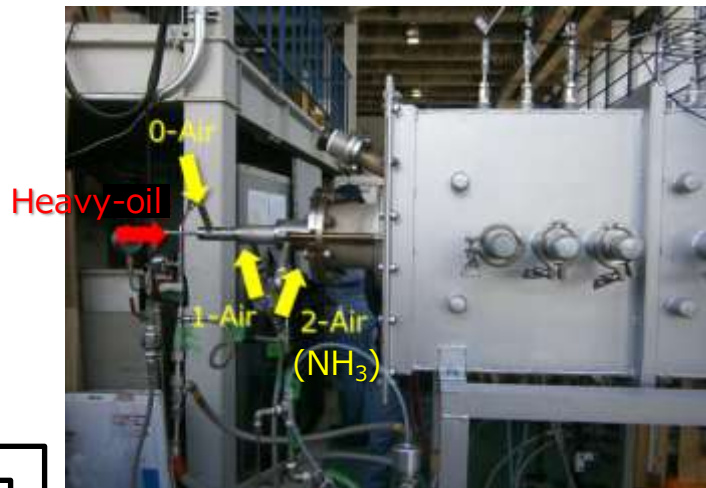
➤ Clinker minerals, reaction rate didn't depend on the gas conditions.

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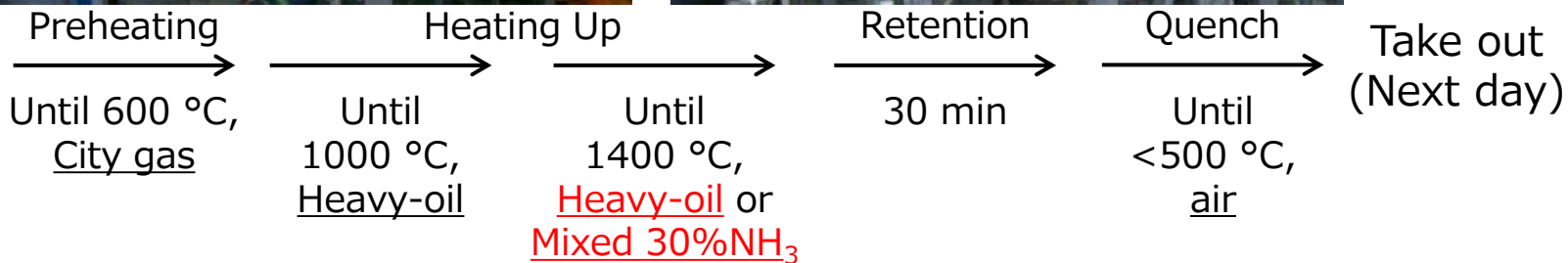
# 【Experiment 2】 $NH_3$ heavy-oil co-fired clinker

## □ Procedure

10 kW Test Furnace Inner Size (mm) : L.1500×W.300×H.300



Clinker Injection



Test furnace

# [Experiment 2] Chemical analysis, physical testing

## □ Chemical analysis

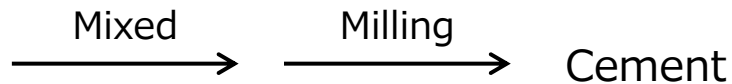
**Minerals** (XRD/Rietveld)

**free-CaO** (JCAS-01(1997), Ethylene glycol dissolution method)

## □ Physical testing (JIS R 5201)

◆ Cement clinker

◆  $\text{CaSO}_4 \cdot 2\text{H}_2\text{O}$

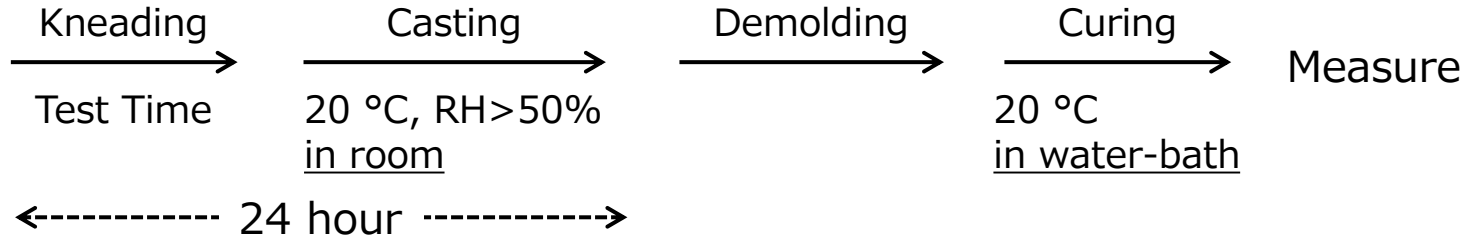


Test Piece Size (mm) : L.160×W.40×D.40

◆ Cement

◆ Sand

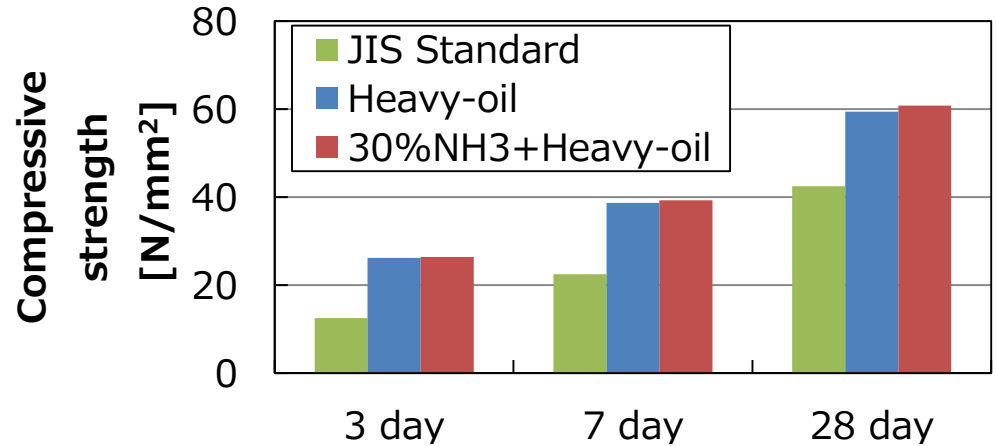
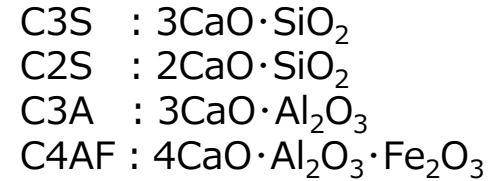
◆ Water



Measured age : 3 day, 7 day or 28 day

# 【Results】Clinker Minerals and Cement Strength

Firing conditions	Clinker minerals (wt.%)				
	f-CaO	C3S	C2S	C3A	C4AF
Heavy-oil	0.19	49.4	30.5	8.2	9.5
30%NH <sub>3</sub> +Heavy-oil	0.18	50.2	29.9	8.3	9.5



- f-CaO less than 0.2 wt. %, same clinker minerals
- No influence of conditions on compressive strength, satisfying JIS

- We' ve done 2 basic experiment toward applying  $\text{NH}_3$  energy for cement process
- The main findings of this work are as follows.
  - ✓ The reaction rate of clinker didn't depend on the gas conditions (**exhaust-gas atmosphere**).
  - ✓ There was no difference in minerals of clinker and compressive strength of cement on the firing conditions (**only heavy-oil or mixed  $\text{NH}_3$** ).



*Thank you for your attention !*

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Osaka University to lend the test furnace and support for driving it.