

Low-Pressure Electrolytic Ammonia (LPEA) Production via Polymer–Inorganic Composite (PIC) Membrane



Critical Challenges. **Practical Solutions.**

NH₃ Fuel Association Annual Conference
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Project Partners



NDSU MECHANICAL
ENGINEERING

UND UNIVERSITY OF
NORTH DAKOTA
CHEMISTRY



Office of
ENERGY EFFICIENCY & RENEWABLE ENERGY



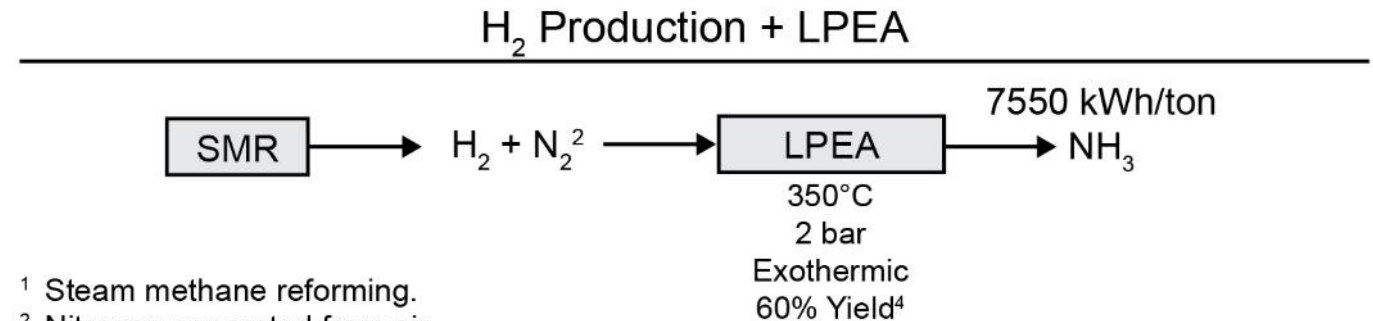
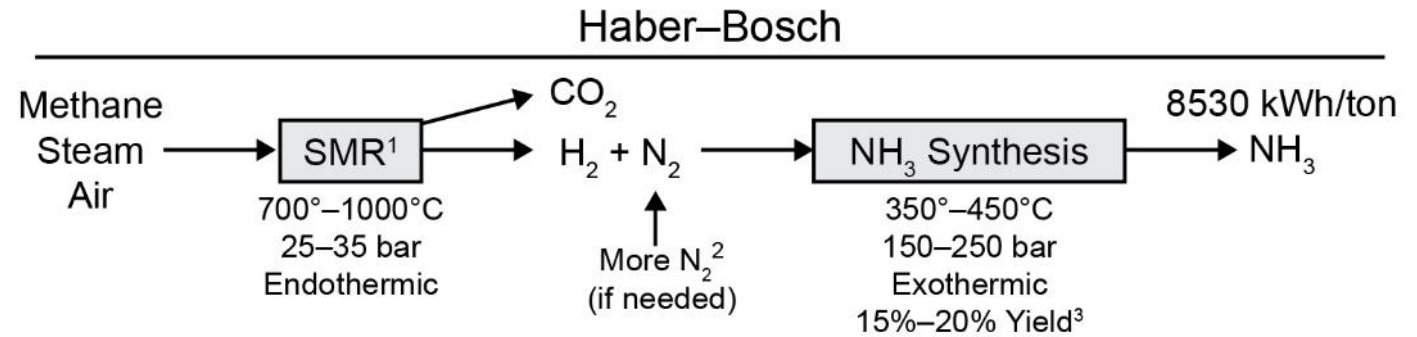
**Demonstrate at least 12%
LPEA energy input reduction
versus HB-based processes:
8530 to 7550 kWh/ton NH₃**

**Demonstrate LPEA reduced
capital/operating cost and turn
down/on/off flexibility**

**Key to achieving goals is high-
temperature (350°C) high-
proton-conductivity gas-
impermeable polymer-
inorganic composite (PIC)
proton exchange membrane**

Project Goals

EERC TA53502.AI



¹ Steam methane reforming.

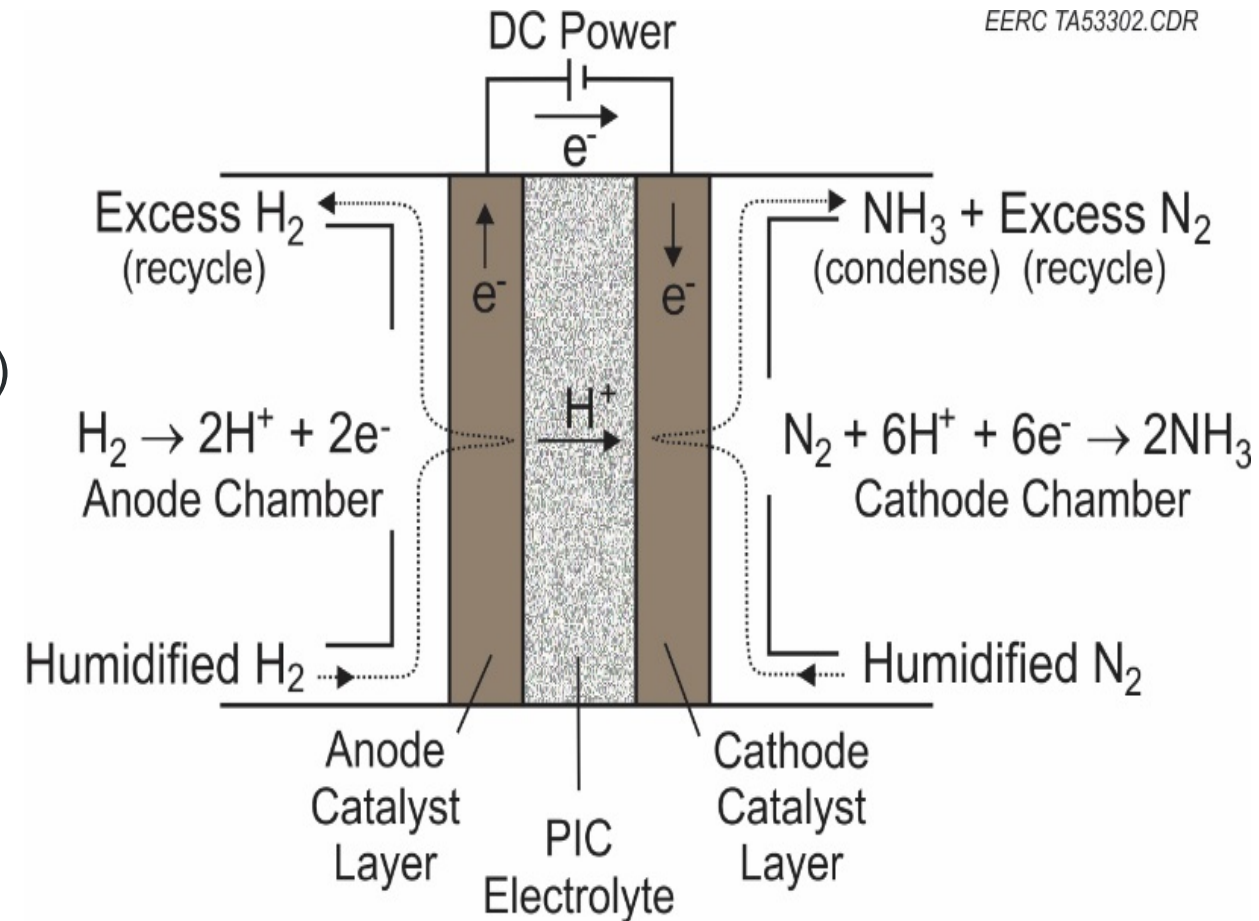
² Nitrogen separated from air.

³ Single-pass yield based on hydrogen conversion.

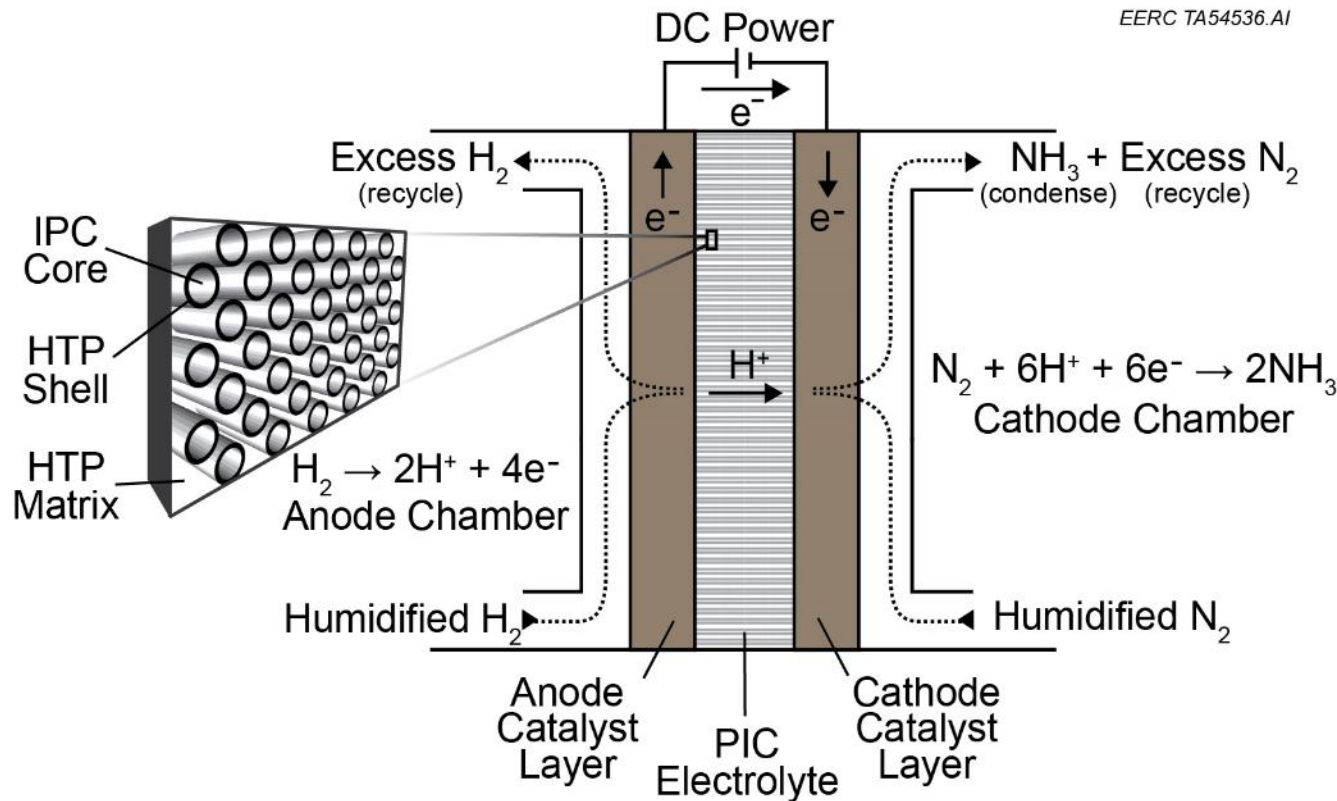
⁴ Targeted single-pass yield based on current efficiency of 65% at current density of 0.25 A/cm².

Patented LPEA process based on initial PIC membrane

- EERC developed and patented
 - U.S. Patent 9,005,422 B2
 - U.S. Patent 8,152,988
- Based on PIC membrane, which comprises:
 - Inorganic proton conductor material capable of 10^{-2} siemens/centimeter (S/cm) proton conductivity at 350°C
 - High-temperature polymer matrix for gas-tight seal
- Key LPEA performance attributes
 - Solid state simplicity
 - Economic turn down/on/off capability
 - Modularity/scalability



Advanced PIC Membrane



- Advanced compositing process yields nanofibers comprising “core” of inorganic proton conductor (IPC) and “shell” of high-temperature polymer (HTP)
- Core-shell IPC-HTP nanofibers aligned within HTP matrix function as proton-conducting “wires”
- Resulting PIC membrane is gas-tight with high-proton-conductivity at 350°C operating temperature, required for commercially relevant NH_3 production rate

PIC Proton Exchange Membrane Performance Targets

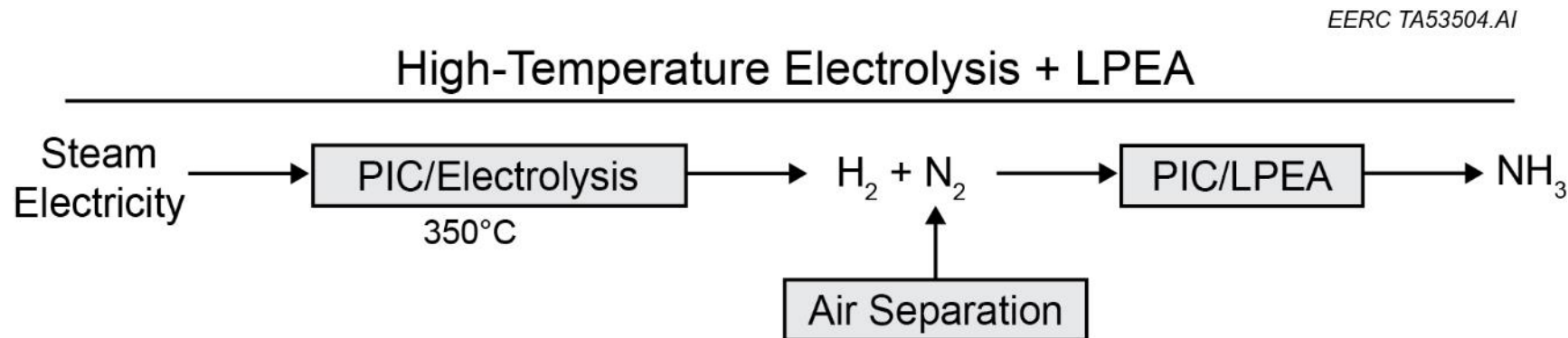
- Proton conductivity of $\geq 10^{-2}$ siemens/centimeter (S/cm) at 350°C
 - Gas permeability of $< 2\%$ at 350°C
 - Ability to sustain 10^{-2} S/cm proton conductivity for at least 1000 hours
 - Mechanical strength (at 350°C) comparable to that of commercial PEM electrolyzer membrane
 - As measured in membrane–electrode assembly (MEA) at 350°C:
 - Current efficiency of $\geq 65\%$ for ammonia formation at current density of ≥ 0.25 amps/centimeter²*
 - Ammonia production efficiency of $\geq 65\%^*$
 - $\leq 0.3\%$ performance degradation per 1000 hours operation*
- * U.S Department of Energy-specified performance target**

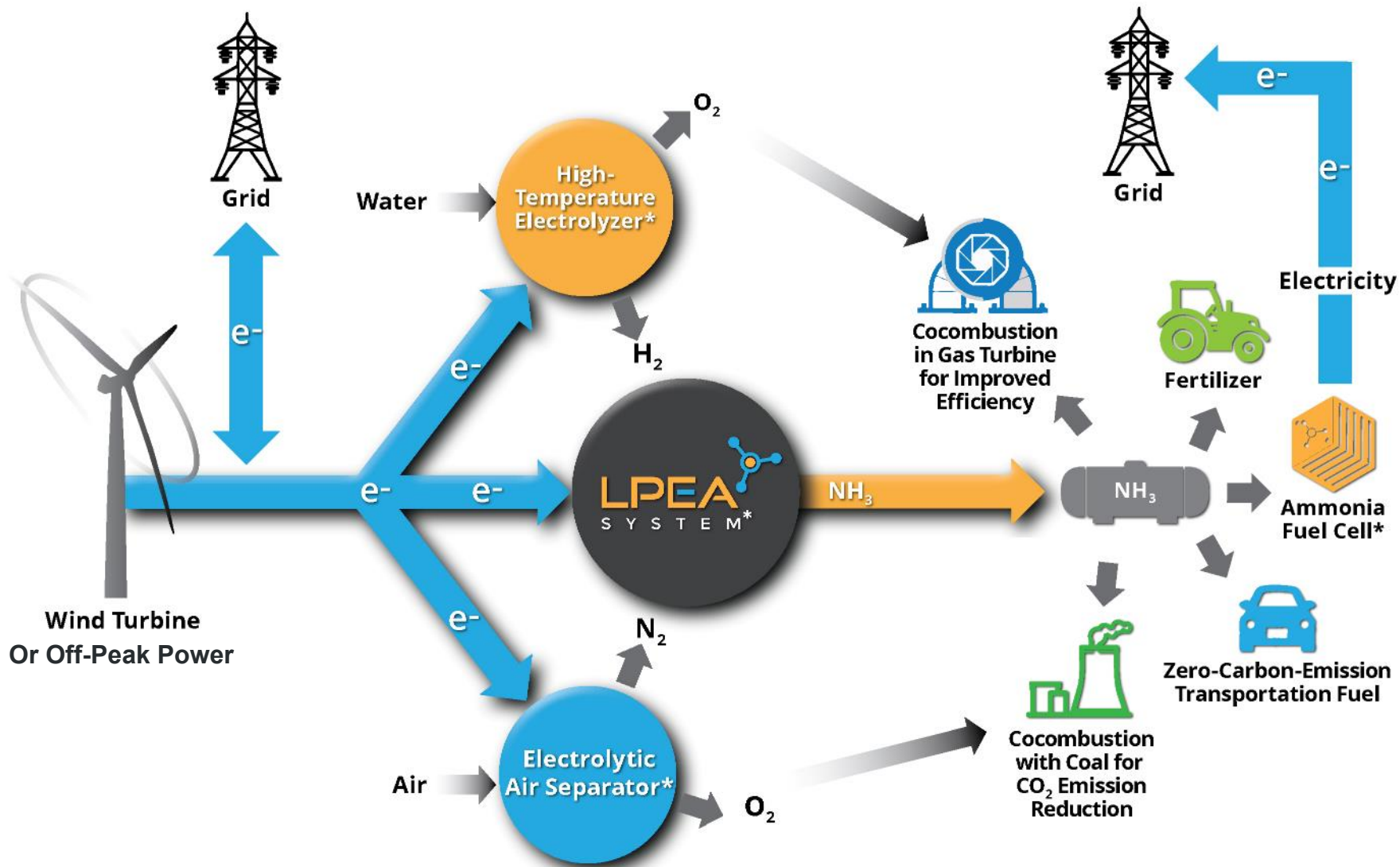
LPEA Techno-Economic Evaluation

- Establish LPEA input energy requirement based on results of extended system operation tests (minimum 12% reduction versus HB is targeted)
- Derive (from project data) complete LPEA system capital and operating cost estimates (on per-annual-ton-ammonia-production-capacity basis) at distributed scales selected to match renewable energy generation capacities specified by North Dakota utilities
- Project overall per-ton ammonia production costs at selected North Dakota locations
- Compare LPEA per-ton cost with per-ton cost of HB-produced delivered ammonia

Commercialization

- Use techno-economic analysis results to secure arrangements with North Dakota utility or ammonia production facility for LPEA pilot-scale demo
- Use demo results to negotiate nonexclusive licenses with engineering/design firms that service ammonia, chemical, power industries
- Use demo results to market LPEA as:
 - Option for integration into existing ammonia supply chain to replace portions of and/or supplement current HB infrastructure
 - Means for monetizing renewable energy and/or utilizing low-cost off-peak power.
- PIC membrane may also be applicable to high-temperature low-energy electrolysis for hydrogen production (below)





Ammonia: Fuel and Fertilizer

* Technology based on EERC-NDSU-developed polymer-inorganic composite (PIC) electrolytic membrane.

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